Response to Comments on Audit Report on Measures for Mitigating Hazard to Life (Issue 2)

1. Comments from Environemtnal Protection Department dated 6 October 2023 via Fax......2

No.	Comments	Response
1.	General – Please state explicitly (e.g. S.1.2, cover letter, etc.) if the scope of the Project covers Stage 1 of the Tsueng Kwan O Desalination Plant (DP1) only.	The relevant text has been amended accordingly.
2.	Report Cover – Please clarify whether the Report is intended for Stage 2 of the Tseung Kwan O Desalination Plant.	The report is intended for the first stage of the desalination plant. Report cover has been amended accordingly.
3.	Table 2-1 and 2-2 – (a) "Audit Results" – According to Condition 2.20 of the EP, the audit report should certify the implementation of design requirements / measures recommended in the Detailed Design Plan (DDP). However, it is noted from the audit results that the implementation status of some measures are stated as "will be installed"/ "will be provided" / "being installed"/ "construction in progress" / etc., which suggests that the requirements / measures are yet to be implemented. Please review and clarify.	The audit results have been updated to clarify that the measures have been implemented.
	(b) "Audit Results" (last column) – It appears that some of the audit results does not confirm the implementation of the requirements / measures as required by Condition 2.20 of the EP, but indicates that there is no change to the recommendation presented in DDP and provide supplementary information only. Please provide the audit results with explicit confirmation of the implementation of requirements / measures if applicable.	The audit results have been updated to clarify that the measures have been implemented.
4.	Table 2-2 – (a) Item 1.3 (last column) – It is noted from the audit result that the provided on-site chlorine generation (OSCG) building volume is 5450.38 m3, which exceeds the design requirements stated in the 2017 ERR (i.e. 4000 m3) and the recommendation in the 2021 DDP (i.e. 3800 m3). In view that the OSCG building volume of 4000 m3 was a design assumption for computation of the chlorine release rate in the 2017 ERR as stated in the 4 th column, please clarify whether such increase of OSCG building volume was reviewed / approved in any of the EIAO documents of the Project (e.g. those listed in Condition 1.7 of the EP). If not, another ERR should be submitted	Please be clarified that the volume of 4,000 m ³ is not a design requirement. It is not an upper limit nor a lower limit but is a design assumption used in the 2017 ERR. Text has been added in Table 2.2 (Item 1.3) to adequately address the environmental implications of such change and explain to the public that the change will not cause any adverse hazard to life impact. Implications of the changes have also been reviewed in S13.2.11 of a separate ERR (Issue 1) for "Agreement No. CE 92/2022 (WS) Second Stage of Desalination Plant at Tseung Kwan O - Investigation, Design and Construction" (2023 ERR) submitted to EPD. Based on the technical comments

1. Comments from Environemtnal Protection Department dated 6 October 2023 via Fax

No.	Comments	Response	
	separately to review the implication of the revised design (e.g. whether the chlorine release rate would be changed due to the increase in volume of the OSCG building) before implementation.	received from the EPD on 18 Oct, 1 Nov and 8 Nov 2023, EPD has no comment on S13.2.11 of the 2023 ERR, which states that such change of building volume would not cause additional adverse hazard to life impact.	
(b) Item 4.1 (last column) – Please confirm whether hoses and couplers for transfer of the concerned chemicals are different in size as required.		Confirmation has been added in the revised report.	
	(c) Item 4.2 (4 th column) – It seems that the design value in the approved DDP is "about 300m". Please review.	Amended accordingly.	
	(d) Item 5.7 (4 th column) – It seems illogical that recommendations in 2021 DDP was based on the explosive delivery route provided by CEDD in 2023. Please review.	The typo "in 2023" has been deleted.	
5.	S.3.1.1.1 – We have reservation to the conclusion at this stage as some of the design requirements / measures are not "being implemented" yet.	Updated information has been provided in the revised report for your review.	

ISSUE 3

AUDIT REPORT ON MEASURES FOR MITIGATING HAZARD TO LIFE

First Stage of Desalination Plant at Tseung Kwan O

BINNIES PROJECT NO. 4110400/40.0000.11A

Report Authorized For Issue By:

anstrato

For and on Behalf of Binnies Hong Kong Limited

PREPARED FOR

Water Supplies Department



DOCUMENT CONTROL		Contract No. 13/WSD/17		No: 4110400/40.0000.11A	
AMENDMENT RECORD		Trist Stage of Desaination Plant at Tseung Kwan O		Prepared By: Binnies	
Audit Report on Measures		Client: Water Supplies Department		Initials: AC	
for Mitig	ating Hazard to Life	Issue	Description	Date: 29 April 2024	T . '4' - 1 -
Pages	Date	No.	Description		Initials
All	August 2023	1	Issue 1		AC
All	September 2023	2	Issue 2		AC
All	April 2024	3	Issue 3		AC

First Stage of Desalination Plant at Tseng Kwan O

Environmental Certification Sheet for Further Environmental Permit (FEP) No. FEP-01/503/2015/B and Environmental Permit (EP) No. EP-503/2015/B

Name of this Document: Auc	lit Report on Measures for Mitigating Hazard to Life
Prepared by: Bin	nies Hong Kong Limited
Date of Report:29 /	April 2024

Reference FEP and EP Condition: Condition 2.20

No later than 3 months before the commencement of operation of the Project, 4 hard copies and 1 electronic copy of an audit report shall be submitted to the Director for record to certifying the implementation of design requirements / measures recommended in the Detailed Design Plan approved under Condition 2.12 of this Permit. Before submission to the Director, the audit report shall be certified by the ET Leader and verified by the IEC as conforming to the recommendations contained in the Detailed Design Plan approved under Condition 2.12.

Environmental Team (ET) Certification:

I hereby certify the above reference document in accordance with Condition 2.20 of FEP No. FEP-01/503/2015/B and EP No. EP-503/2015/B.

Jacky LEUNG	Refer to the separate		
ET Leader	certification letter	Date:	30 April 2024
Acuity Sustainability Consulting Limited	Signature		00 mpin 202 i

Independent Environmental Checker (IEC) Verification:					
I hereby verify the above reference document in accordance with Condition 2.20 of FEP No. FEP-01/503/2015/B and EP No. EP-503/2015/B.					
Serena SHEK Refer to the separate					
IEC	verification letter	Date:	30 April 2024		
Lam Environmental Services Limited Signature					

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Appendix B	Design Requirements and Measures for CO ₂ Storage
Appendix C	Separation Distances Between Major Facilities in DP1

1 Introduction

1.1 Background

- 1.1.1 The desalination plant at Tseung Kwan O (TKO) Area 137 (**the Project**) involves 2 stages. Stage 1 of the Project (DP1) involves a water production capacity of 135,000 cubic meters (m³) per day. Stage 2 of the Project (DP2) involves an additional water production capacity of 135,000 m³ per day. The overall capacity of the Project would be 270,000 m³ per day at the ultimate stage.
- 1.1.2 An Environmental Impact Assessment (EIA) study for the Project was completed in accordance with the EIA Ordinance (EIAO) during the Feasibility Study (FS) stage of the Project. The EIA Report for the Project (Register No.: AEIAR-192/2015) was approved on 4 November 2015 under the EIAO (**the 2015 EIA**). The Environmental Permit (EP) (No: EP-503/2015), covering the construction and operation of Project, was granted on 4 December 2015.
- 1.1.3 Following the approval of the 2015 EIA, the Project design was further reviewed, and several design changes were identified. An environmental review was then carried out to address the environmental impacts arising from the design changes and to support the necessary Variation of Environmental Permit (VEP) application for the Project. The findings of the environmental review are presented in the report "Agreement No. CE 8/2015 (WS) First Stage of Desalination Plant at Tseung Kwan O Investigation, Design, Construction. Environmental Review Report Variations for Design Changes (Issue 2)" issued on 3 November 2017" (the 2017 ERR). Amendment of the EP was applied under the EIAO on 5 January 2018. The amended EP (No: EP-503/2015/A) was subsequently granted on 26 January 2018.
- 1.1.4 On 29 November 2019, the Contractor of DP1 submitted the application for Further Environmental Permit (FEP) to the Environmental Protection Department (EPD) under Section 12 of the EIAO. The FEP (No. FEP-01/503/2015/A) was granted to the Contractor on 20 December 2019.
- 1.1.5 Further amendment of the EP and FEP was applied on 12 March 2024. The latest amended EP (No. EP-503/2015/B) and FEP (No. FEP-01/503/2015/B) were granted on 3 April 2024.
- 1.1.6 In accordance with Condition 2.12 of the latest EP and FEP, a Detailed Design Plan (DDP) for Storage of Chlorine and Carbon Dioxide was prepared for the Project and submitted to EPD on 17 March 2020. With incorporation of all comments received from the EPD, the DDP was approved by EPD on 17 August 2021. The 2021 DDP provides the design details of DP1 and assumes that the design of DP2 would remain the same as the reference design adopted in the 2017 ERR. The 2021 DDP also compares the design details of the Project against the design requirements / measures specified in Table 1 of the EP / FEP and in the 2017 ERR.

1.2 Scope and Purpose of this Audit Report

1.2.1 This Audit Report is prepared for the first stage of the Tseung Kwan O Desalination Plant (DP1) in accordance with Condition 2.20 of the FEP and EP for certifying the implementation of design requirements / measures recommended in the 2021 DDP approved under Condition 2.12 of the FEP and EP, and for submission to the EPD for record. This Audit Report has been certified by the Environmental Team Leader and verified by the Independent Environmental Checker (IEC) as conforming to the recommendations contained in the 2021 DDP approved under Condition 2.12 of the FEP and EP.

1.3 Report Structure

1.3.1 The Report Structure is as follows:

Section 1	Introduction
Section 2	Audit Results
Section 3	Conclusion

2 Audit Results

2.1.1 DP1 is under construction stage and is scheduled for completion and commissioning by late December 2023. DP2 is currently under the investigation and design stage. DP2 is scheduled for construction in 2024 and commissioning in 2027. The audit results for certifying the implementation of design requirements / measures in DP1 as recommended in the 2021 DDP are presented in **Table 2-1** and **Table 2-2**.

Table 2-1 Audit Results for Implementation of Design Requirements / Measures for Chlorine and Carbon Dioxide Storage Recommended in the FEP and 2021 DDP

No.	Types of Storage	Design Requirements/Measures in FEP	Recommendations in 2021 DDP	Audit Results - A
1.	Chlorine Store			
1.1	Chlorine storage quantity in the chlorine	No more than 37 tonnes in 1-tonne drums	The Project will adopt the On-site Chlorine Generation	OSCG has been
	store	Larger than 4200 m ³	use of OSCG system avoids the importation of liquid chlorine	of liquid chlorine.
1.2	Volume of chlorine store		and the need for stocking/ on-site storage of chlorine (i.e.,	in the OSCG buildi
1.3	Design and layout of chlorine store	The chlorine store shall be designed in a way such that the average number of drums ruptured in the worst-case scenario during earthquake should be no more than 6.	Potential Hazardous Installation) whereby intrinsically eliminating the hazard due to transport (on-site and off-site) use, and storage of liquid chlorine, and thus reducing the risk to human life and the development constraints in the	Appendix A-1 and
1.4	Separation distance between, the chlorine store and explosive trucks / TKO Area 137 Pier	The setback distance between the chlorine building and explosive trucks / TKO Area 137 Pier shall provide sufficient clearance **(see remarks below) so that the overpressure resulting from explosion of explosive trucks or the explosives offloading operation that reaches the chlorine building is less than 2 psi.	vicinity.	
1.5	Separation distance between the chlorine store and any one of the site boundaries (except for the site boundary adjacent to the Clear Water Bay Country Park)	More than 100m		
2	Carbon Dioxide Store			
2.1	Maximum number of carbon dioxide storage tank	16 units	5 units in DP1	The CO ₂ storag recommendations drawing and phot B-2.
2.2	Type of storage tank	Vacuum insulated, double containment	Vacuum insulated, double containment	The CO ₂ storag recommendations double containme in Appendix B-3 .
2.3	Storage tank capacity	No more than 100 tonnes per tank	Capacity 100 tonnes per tank	The CO ₂ storag recommendations indicated in Appe
2.4	Pressure relief system of carbon dioxide storage tank	Pressure protection for the inner vessel shall be provided by 2 sets (1 duty and 1 stand-by) of pressure protection devices. Each set of pressure protection device will be composed of 2 independent pressure relief valves. The pressure relief valves system will be designed to avoid the common mode failure such that the risk of common mode failure is negligible.	Two sets of pressure protection devices will be provided at inner vessel. Each will compose of two independent pressure relief valves and will be designed to avoid common mode failure.	The CO ₂ tanks hav 2021 DDP and Instrumentation tanks and related presented in the 2 reproduced in Ap of pressure relief
		The pressure protection device on the outer vessel shall be a plate relief device. The plate relief device will be a standard installation in accordance with industrial standards (EN 13458 Part 2 Annex 1).	Pressure relief valves will be provided on the outer vessel, which will be plate relief valves and will be of EN 13458 Part 2 standard compliant.	The CO ₂ storag recommendations relief system imp Appendix B-6 an
2.5	Pressure relief system of carbon dioxide road tanker	Pressure protection for the inner vessel shall be provided by 2 sets (1 duty and 1 stand-by) of pressure protection devices. Each set of pressure protection device shall be composed of 2 independent pressure relief valves. The pressure relief valves system shall be designed to avoid the common mode failure such that the risk of common mode failure is negligible.	Two sets of pressure protection devices will be provided on the inner vessel. Each will compose of two independent pressure relief valves and will be designed to avoid common mode failure.	Pressure protection following the record P&ID of CO ₂ Road presented in the 2 is reproduced in A
2.6	Separation distance between the carbon dioxide storage area and explosive trucks / TKO Area 137 Pier	The setback distance between the carbon dioxide storage area and explosive trucks / TKO Area 137 Pier shall provide sufficient clearance so that the overpressure resulting from explosion of explosive trucks or the explosives offloading operation that reaches the carbon dioxide storage area is less than 2 psi.	The maximum offloading capacity to the explosive offloading pier at TKO Area 137 is 5,000 kg TNT equivalent explosives The maximum capacity per explosive truck from the explosive offloading pier at TKO Area 137 is 1,750 kg TNT equivalent explosives. According to 2017 ERR and based on the formula given in the Queensland Explosives Information Bulletin 50 Version 4 (current) Section 12 (the Bulletin 50) and referring	The as-built loca Appendix C) follo also met the relev t

Actual Provisions for DP1 and Records

n implemented in DP1 in accordance with the of the DDP to replace the importation, storage and use The OSCG main skids (2 trains) are currently positioned ing for DP1. Drawing and photo records are provided in the **Appendix A-2**.

ge tanks have been implemented following the s in 2021 DDP. Only 5 units are installed in DP1. Layout to records are provided in **Appendix B-1** and **Appendix**

ge tanks have been implemented following the s in 2021 DDP. Storage tanks are vacuum insulated with ent. Specifications of CO2 tanks installed in DP1 are given

ge tanks have been implemented following the s in 2021 DDP. Capacity of each tank is 100 tonnes as e**ndix B-1**.

ve been implemented following the recommendations in in accordance with the Detailed Process and Diagrams (P&IDs) of Remineralization CO₂ storage d systems and details of the pressure relief system as 2021 DDP. Relevant information from the 2021 DDP is **pendix B-4** and **Appendix B-6** for record. Photo record valve is included in **Appendix B-7**.

ge tanks have been implemented following the s in 2021 DDP. Details and photo record of the pressure lemented for the CO₂ storage tanks in DP1 are given in d **Appendix B-7**.

ion devices have been implemented for the CO₂ tanker commendations in 2021 DDP and in accordance with the d Tanker and details of the pressure relief system as 2021 DDP. The relevant information from the 2021 DDP Appendix B-5 and Appendix B-6 for ease of reference.

ation of the CO₂ storage area in DP1 (as indicated in ows the recommendations in the 2021 DDP, and hence vant separation requirement of the EP and FEP.

No.	Types of Storage	Design Requirements/Measures in FEP	Recommendations in 2021 DDP	Audit Results - A
			to Kingery-Bulmash Blast Parameter Calculator on the website of International Ammunition Technical Guidelines, United Nation, the 2-psi overpressure zone for 5,000 kg and 1,750 kg TNT equivalent explosives is within 178 m and 125m from the explosion source respectively.	
			The liquid carbon dioxide (CO_2) storage area in DP1 is over 300m from the explosive offloading pier, which is greater than the maximum hazard distance or the 2psi overpressure zone of 178m from the explosive source. The CO_2 storage area in DP1 would have sufficient clearance from the explosive offloading pier. The CO_2 storage area in DP1 would not be impacted by the explosive explosion at the pier.	
			Based on the explosive delivery route provided by CEDD at the time of preparing the 2021 DDP, the CO ₂ storage area in DP1 is located outside the 2psi overpressure zone of the explosion of the explosive delivery truck. The CO ₂ storage area in DP1 would not be impacted by the road transport of explosives.	
2.7	Separation distance between the carbon dioxide storage area and any one of the site boundaries (except for the site boundary adjacent to the Clear Water Bay Country Park)	More than 100m	The CO ₂ storage in DP1 is situated at more than 100 m away from both northern and western boundaries of the desalination plant.	The as-built CO2 2021 DDP. It is sit western boundar
		Trycock for overfilling alarm and warning shall be provided on carbon dioxide storage tanks.	Trycock valves will be provided for overfilling alarm and warning on CO2 storage tanks.	Trycock valves ha photo records of Appendix B-9 .
2.8	Other safety features of carbon dioxide storage tanks and the facilities	High level alarm shall be provided to operating staff at control room for liquid level monitoring and warning.	High level alarm will be provided and connected to main control room.	High level alarm High level alarm i
		Fencing shall be provided surrounding the carbon dioxide facilities.	Security fence will be provided around CO2 storage area.	Security fence ha in Appendix B-1

Table 2-2 Audit Results for Implementation of Design Requirements / Measures for Chlorine and Carbon Dioxide Storage Recommended in the 2017 ERR and 2021 DDP

No.	Parameters	Design Requirements / Measures in 2017 ERR	Recommendations in 2021 DDP	Audit Results - A
1	On-site Chlorine Generation	n		
1.1	Chlorine generation rate	The ultimate chlorine generation rate (including both Stage 1 and Stage 2 works) is 2250 kg per day. Two OSCG systems, each with capacity of 1125 kg per day, will be installed in 2 stages in 2 separate buildings.	No changes to these assumptions are proposed.	The current OSCO kg/d per train x 2 data sheet extrac Appendix A-3 . T additional hazard
1.2	Ventilation rate	6 air change per hour (ACPH)	No change to the ventilation rate is proposed.	Forced ventilation within the OSCG b

Actual Provisions for DP1 and Records

storage area in DP1 follows the recommendations of tuated at more than 100 m away from both northern and ries of the desalination plant as shown in **Appendix C**.

ave been provided on the CO2 storage tanks. Details and f the trycock valves are given in **Appendix B-8** and

has been provided and connected to the control room. is indicated in the P&ID in **Appendix B-4**. as been installed around the CO₂ Storage area as shown **0**.

Actual Provisions for DP1 and Records

CG design ultimate production for DP1 is 426 kg/d (213 2 trains) for DP1. Supporting information including cted from the material submission is given in The reduced production rate would not induce rd to life impact.

on of minimum 6 ACPH is provided for 7 nos. of rooms building for DP1 as follows.

No.	Parameters	Design Requirements / Measures in 2017 ERR	Recommendations in 2021 DDP	Audit Results - Actual P	rovisions fo	r DP1	and Record	s
				Room Name	Provision	ACH	Ventilation Max. Room Design Temperature, °C	Relative Humidity, %
				Scrubber Room	MV	6	40	Uncontrolled
				Big Bag Salt Store Room	MV	6	-	Less than 50%
				Electrolyser Skid Stream Room	MV	6	40	Uncontrolled
				Equalisation Tank and Neutralisation Tank Room	MV	6	40	Uncontrolled
				Filtered Brine Tank Room	MV	6	-	Uncontrolled
				Chlorinators Room	MV	6	40	Uncontrolled
				DG Store 4 Class 8 (Sodium Hypochlorite Store)	MV	6	-	Uncontrolled
				Air Conditioning is provid	led for Electi	rical ro	oom of OSCG	building.
				Natural ventilation is pro Hydrochloric Acid room a	vided for the and Sodium H	Sodiu Iydrox	m Bisulphite tide room of	e room, OSCG building.
				Supporting documents in in Appendix A4 and App	cluding data endix A5.	sheet	and drawing	are provided
1.3	Volume of each OSCG building	4000 m ³	Proposed Design Value: 3800 m ³ Hazard Implications: In the 2017 ERR, the 10-minute average chlorine release rates to atmosphere (due to accidental indoor chlorine release) were computed by the PHAST model with reference to the building volume of 4000 m ³ and the 6 ACPH ventilation rate. In view that the ventilation rate and chlorine generation rate in each OSCG building and the associated indoor chlorine release rate at source as assumed in the 2017 ERR would remain unchanged, the chlorine release rates to atmosphere would not be significantly affected by the slight reduction of the building volume. In addition, the chlorine risks as predicted in the 2017 ERR are well within the acceptable levels with great safety margins from the assessment criteria. The slight reduction of the building volume would not cause any significant implication on the overall conclusion of the 2017 ERR on the chlorine hazards.	As-built Building Volum Electrolyser skid stream Entire OSCG Building = 5- Supporting information is Hazard Implications: The skid stream room. Its ven the daily chlorine product release rate at source wo kg per day as assumed in release rates to atmosphe in the skid room volume. 2017 ERR are well within from the assessment critic not cause any adverse im 2017 ERR and would not	ne: room = 4323 450.38 m ³ s given in Ap ne OSCG skids tilation rate ction rate and uld be reduce the 2017 ER ere would no In addition, to the acceptal eria. The chan plication on lead to any u	.10 m ³ pendi s are s would d the a ed by r R to 42 t be in the pre- ble lev nge of the chl unacce	x A-6 . tored in the or ssociated inconstruction nore than 50 26 kg per day creased due edicted chlor els with grea the building orine risk pr ptable chlori	electrolyser e 6 ACPH) and loor chlorine 1% from 1,125 7. The chlorine to the increase ine risks in the t margins volume would resented in the ne hazard.
2	Chlorine Gas							
2.1	Discharge of chlorine gas to the atmosphere	No vent pipe will be provided for direct discharge to the atmosphere	No change to this design requirement is proposed.	This design requirement vent pipe for direct disch There are three types of v building, which are hydro from scrubber as shown	has been pro arge of chlor vents dischar ogen vent, tan in Appendix	perly i ine gas ging to nk air v A-7 .	implemented s to atmosph o atmosphered vent and trea	l. There is no ere. e in the OSCG ted air vent
2.2	Safety measures	 Chlorine detectors Chlorine scrubber system Activation of recycle damper when chlorine scrubber is in operation 	All these safety measures will be adopted in the proposed design.	Safety measures have bee recommendations of 202 and EPD's "no objection" A-8 to Appendix A-11 .	en implemen 1 DDP. Pleas reply to the j	ted fol e refer propos	lowing the to supportir ed scrubber	ng information in Appendix
2.3	Separation distance between the centre of OSCG building and the nearest site boundary	Greater than 30 m	 Over 100 m for OSCG in DP1 > 30 m for OSCG in DP2 	The OSCG building in DP2 recommendations of 202 document including the E record in Appendix C.	l has been im 1 DDP. Pleas BIM screen sh	ipleme e refer iot in <i>F</i>	ented followi to the suppo Appendix A-	ng the orting 12 and photo

No.	Parameters	Design Requirements / Measures in 2017 ERR	Recommendations in 2021 DDP	Audit Results -
2.4	Separation distance between the exhaust point / louvers of OSCG buildings and the nearest site boundary	Greater than 30 m	 Over 100 m for OSCG in DP1 > 30 m for OSCG in DP2 	The OSCG buildi have been imple Please refer to t in Appendix A -
3	Hydrogen Release		·	
3.1	Discharge of hydrogen gas to the atmosphere	Individual vent pipe will be provided for each generator	No change to this design requirement is proposed.	Individual hydro indicated in App
3.2	Concentration of hydrogen gas for discharge to the atmosphere	1% of Lower Flammability Limit (LFL) for hydrogen	No change to this design requirement is proposed.	Dilution blower less than 1% by be raised when hydrogen conce has been impler OSCG skids 1 & 2 Please refer to t 8, Appendix A -
3.3	Hydrogen explosion due to failure of OSCG units	The hazard distance of hydrogen explosion from the OSCG skid was estimated to be 11m for overpressure of 2 psi. Under the reference design, sufficient separation was provided between the chemical tanks and OSCG units to avoid simultaneous failure of tanks containing incompatible chemicals.	Sufficient separation will be provided between the chemical tanks and OSCG units in DP1 to avoid simultaneous failure of tanks containing incompatible chemicals,	The chemical ta building of DP1 BIM model sepa Appendix A-15 the BIM model.
4	Sodium Bisulphite (NaHSO3) Assessment		
4.1	Safety measures to avoid right product delivered into the wrong tank.	Hoses and couplers for transferring of NaHSO ₃ , hydrochloric acid (HCl), ferric chloride (FeCl ₃), sulphuric acid (H ₂ SO ₄) and citric acid (C ₆ H ₈ O ₇) are different in size to avoid connecting road tankers of incompatible chemicals to corresponding storage tanks.	No change to the safety measure is proposed.	According to Co ($C_6H_8O_7$) storage Hoses and coup are in different s recommendatio 42).
		Warning signs will be displayed at the inlet of each storage tank to show chemical name and to warn the potential hazards of mixing incompatible chamicals	No change to the safety measure is proposed.	Warning signs h recommendatio
		NaHSO ₃ , sodium hypochlorite (NaOCl), HCl, FeCl ₃ , H ₂ SO ₄ and C ₆ H ₈ O ₇ will be delivered by road tankers.	No change to the safety measure is proposed.	The safety meas recommendatio information in A provision of filli OSCG Building. A following chemi • NaHSO3 (OS metabisulph Building) • NaOCI (both Chemical Bu • HCI (OSCG E • FeCl3 (Chem • H2SO4 (Che
		HCl, FeCl ₃ , H ₂ SO ₄ and C ₆ H ₈ O ₇ at chemical building will be stored in double containment tanks.	No change to the safety measure is proposed.	Double containr with the recomr approved DG dr

ling and the associated exhaust point / louvers in DP1 emented following the recommendations of 2021 DDP. the supporting document including the BIM screen shot -12 and photo record in Appendix C.

rogen vent has been provided for each generator as **pendix A-7**.

r has been provided to dilute the hydrogen with air to y volume, below LFL. Alarm has been installed and will the in-duct hydrogen monitoring sensor detect the entration higher than 1%. Emergency shutdown (ESD) mented. The ESD panel will be activated and shut off 2.

the supporting drawings and document in **Appendix A-**-13 and **Appendix A-14**.

anks and OSCG units have been installed in the OSCG in accordance with the recommendation in 2021 DDP. aration distance as supporting information is shown in 5. OSCG facilities have been installed in accordance with

ontractor's current design, there is no citric acid ge in DP1.

blers for transferring of NaHSO₃, HCl, FeCl₃ and H₂SO₄ sizes and have been implemented following the ons in the 2017 ERR and 2021 DDP (see **Appendix A**-

have been installed in accordance with the ons in 2017 ERR and 2021 DDP (see **Appendix A-43**).

sure has been implemented in accordance with the ons of 2021 DDP. Please refer to the supporting **Appendix A-16** to **Appendix A-22** showing the ing points for road tankers at Chemical Building and As advised by the potential chemical supplier(s), the icals will be delivered by road tanker

SCG Building) (Note: Powder form of sodium hite will be used for preparing NaHSO3 in Chemical

n Chemical Building and OSCG Building) (photo for uilding is attached in **Appendix A-22**) Building)

nical Building) (photo attached in **Appendix A-22**) emical Building)

ment has been provided for the chemicals in accordance mendations in the 2017 ERR and 2021 DDP. FSD rawings showing the bund arrangement are provided in

No.	Parameters	Design Requirements / Measures in 2017 ERR	Recommendations in 2021 DDP	Audit Results - A
				Appendix A-23 t FeCl ₃ and H ₂ SO ₄ a of all tanks in a co within the bund. ' for HCl, FeCl ₃ and records are given
		HCl, FeCl ₃ , H_2SO_4 and $C_6H_8O_7$ flowing outside of the chemical building will be collected by roadside drains	Floor surface gradient will be used for directing any spillage of HCl, FeCl ₃ , H ₂ SO ₄ and $C_6H_8O_7$ towards the sump within the storage compartment and contained inside the chemical building for further clean-up and proper disposal. Design of the floor gradient shall take account of the viscosity of the chemicals.	Floor surface grad NaOCl rooms, wit recommendation drawings as supp
		Perimeter drain will be installed surrounding NaHSO3, HCl and NaOCl storage compartments at OSCG buildings.	Floor surface gradient will be used for directing any spillage of NaHSO ₃ , HCl and NaOCl towards the sump within the storage compartments and contained inside the OSCG buildings for further clean-up and proper disposal. The floor gradient design of the buildings shall take account of the viscosity of the chemicals.	A-35 and photo r
		Bunds will be provided for all storage compartments	No change to this design measure is proposed.	Bunds have been Supporting inform 33 .
		Double containment will be provided for HCl pipelines in OSCG buildings.	No change to this design measure is proposed.	This design meas containment has spillages outside storage tanks and equal to 100% of double containme room. Supporting Appendix A-40 .
		Alignment of HCl pipeline is away from pipelines for other incompatible chemicals in OSCG building.	No change to this safety measure is proposed.	This design meas alignment of HCl incompatible che
		Floor surface gradient will be used for directing spillage of incompatible chemicals to different locations such that HCl will be collected to a separate drain system.	No change to this safety measure is proposed in the latest design.	This design meas gradient has beer incompatible che collected to a sep drawings as supp
		Only one storage tank will be connected to delivery pipeline at any one time to minimize the amount of spillage.	No change to this design measure is proposed.	This design meas control valves (or control logic of th one storage tank to minimize the a information in Ar
		Pipe pressure will be continuously monitored. Pumps will be immediately shut down if irregular pressure drops occur.	No change to these design measures is proposed.	This design meas monitoring system bisulphite dosing the control system pump discharge. diagram in Appe
		Vibration sensing system will be installed alone pipelines. Pumps will be immediately shut down if excessive vibration is detected to minimize the amount of leakage through damaged pipelines.	No change to these design measures is proposed.	This design meas sensing system ha bisulphite dosing the control syster Please refer to the A-41 .
4.2	Separation distance between OSCG buildings and chemical building.	380m	Design Value: about300 m Hazard Implications : The separation distance of 380 m in the 2017 ERR is mainly to show that it is one of the safety measures for eliminating the operation error namely "right product delivered into the wrong tank". There is no significant risk implication due to the change in the separation distance from 380 m to 280 m.	Actual Value: 340 Please refer to BI Appendix C .

to **Appendix A-32**. Chemical storage tanks of HCl, are located within bund with capacity equal to 100% compartment which is capable to contain any spillages. The bund works are regarded as double containment d H₂SO₄ at Chemical Building and OSCG Building. Photo n in **Appendix A-33**.

adient has been provided for HCl, FeCl₃, H2 $^{S}O_{4}$, NaHSO₃, ithin the bund in accordance with the

ns of 2021 DDP. Please refer to the architectural porting information in **Appendix A-34** and **Appendix** record of sump pits in **Appendix A-36**.

n provided for the chemical storage compartments. rmation is provided in **Appendix A-23** to **Appendix A-**

sure has been implemented accordingly. Double s been provided for HCl pipeline to contain the e HCl store room. Inside HCl store room, the HCl acid ad pipeline are located within the bund with capacity of all tanks in a compartment. The bund is regarded as nent and will contain the spillages inside HCl store ag information is provided in **Appendix A-37** to

sure has been implemented accordingly. As-built l pipeline is away from pipelines for other

emicals in OSCG building as shown in **Appendix A-38**. sure has been implemented accordingly. Floor surface en provided and will be used for directing spillage of emicals to different locations such that HCl will be parate drain system. Please refer to the architectural porting information in **Appendix A-35**.

sure has been implemented accordingly. Separate open/close) are provided at each tank outlet. The he valves has been developed in a way such that only will be connected to delivery pipeline at any one time amount of spillage. Please refer to the supporting **ppendix A-16** to **Appendix A-22**

sure has been implemented accordingly. Pressure em has been installed at the discharge of the sodium g pumps. The pumps will be tripped to stop running by em when irregular pressure drops are detected at . Please refer to the process and instrumentation endix A-41.

sure has been implemented accordingly. Vibration has been installed at the dosing line of the sodium g pumps. The pumps will be tripped to stop running by em when irregular vibration are detected at dosing line. he process and instrumentation diagram in **Appendix**

0 m (which met the requirement of 2021 DDP) SIM screen shot in **Appendix A-12** and photo record in

No.	Parameters	Design Requirements / Measures in 2017 ERR	Recommendations in 2021 DDP	Audit Results -
5	Liquid Carbon Dioxide (CO2)		
5.1	Number of CO ₂ storage tank	16 units	5 tanks in DP1	The CO ₂ storage recommendation Layout drawing Appendix B-2 .
5.2	Type of storage tank	Vacuum insulated	Vacuum insulated	The CO ₂ storage recommendation vacuum insulate tanks installed in
5.3	Storage tank capacity	100 tonnes per tank	100 tonnes per tank	The CO ₂ storage recommendation indicated in App
5.4	Type of vaporizer	Ambient	Ambient	The CO ₂ storage recommendation Inspection repor
5.5	Transport mode	By road tanker	By road tanker	The transport m of road tanker fil Appendix B-1 .
5.6	Safety measures	CO ₂ storage in double containment	CO2 storage in double containment	The CO ₂ storage recommendation with double com are given in App
		2. set of pressure relief valves (PRVs) on inner containment. The 2 sets of PRVs are connected by a switchover valve. Each set consists of 2 PRVs.	No changes to the design measures are proposed.	The CO ₂ storage recommendation P&IDs of Remine details of the pre- Relevant informa B-4 and Append valve is included
		Plate pressure relief device on outer containment (considered on storage tanks only).	No changes to the design measures are proposed.	Plate pressure re in accordance w photo record of and Appendix B
		Trycock for overfilling alarm and warning	No changes to the design measures are proposed.	Trycock for over accordance with records of the tr B-9 .
		High level alarm to operating staff at control room for liquid level monitoring and warning	No changes to the design measures are proposed.	High level alarm recommendation P&ID in Append
5.7	Separation distance between CO ₂ storage area and the explosive truck during off-site transport	Set back the CO_2 storage with sufficient clearance so that the overpressure resulting from explosion of explosive vehicle during off-site transport that reaches the storage is less than 2 psi.	Based on the explosive delivery route provided by CEDD, the setback distance of the CO_2 storage area in DP1 is located outside the 2psi overpressure zone from the explosive delivery truck. The CO_2 storage area in DP1 would not be impacted by the road transport of explosives.	The as-built loca Appendix C) fol also met the rele
5.8	Separation distance between CO ₂ storage area and the explosive offloading pier	Set back the CO ₂ storage with sufficient clearance so that the overpressure resulting from explosion of explosives at the offloading pier that reaches the storage is less than 2 psi.	The liquid CO ₂ storage areas in DP1 is over 300m from the explosive offloading pier, which is greater than the maximum hazard distance or the 2psi overpressure zone from the explosive source. The CO ₂ storage area in DP1 would have sufficient clearance from the explosive offloading pier.	
5.9	Separation distance between CO2 storage area and site boundary	Approximately 100 m	The CO_2 storage in DP1 is situated at more than 100 m away from both northern and western boundaries of the desalination plant.	The as-built CO ₂ 2021 DDP. It is s and western bou Appendix C .

tanks have been implemented following the ns in 2021 DDP. Only 5 units are installed in DP1. and photo records are provided in **Appendix B-1** and

tanks have been implemented following the ns in 2021 DDP. Storage tanks installed in DP2 are ed with double containment. Specifications of CO2 n DP1 are given in **Appendix B-3**.

tanks have been implemented following the ns in 2021 DDP. Capacity of each tank is 100 tonnes as **bendix B-1**.

tanks have been implemented following the ns in 2021 DDP. The type of vaporizer is ambient. rt is provided in **Appendix B-11**.

node by road tanker has been implemented. Plan view lling point is shown in the CO2 system layout in CO₂ road tanker license is attached in **Appendix B-12**.

tanks have been implemented following the ns in 2021 DDP. Storage tanks are vacuum insulated tainment. Specifications of CO₂ tanks installed in DP1 pendix B-3.

tanks have been implemented following the ns in 2021 DDP and in accordance with the Detailed eralization CO₂ storage tanks and related systems and essure relief system as presented in the 2021 DDP. ation from the 2021 DDP is reproduced in **Appendix dix B-6** for record. Photo record of pressure relief d in **Appendix B-7**.

elief devices have been provided on outer containment ith the recommendations in 2021 DDP. Details and the pressure relief system are given in **Appendix B-6 3-7**.

filling alarm and warning has been implemented in the recommendation in 2021 DDP. Details and photo ycock valves are given in **Appendix B-8** and **Appendix**

has been provided in accordance with the n in 2021 DDP. High level alarm is indicated in the **lix B-4**.

ation of the CO₂ storage area in DP1 (as indicated in lows the design assumption in 2021 DDP, and hence evant separation requirement of the 2017 ERR.

storage area in DP1 follows the recommendations of situated at more than 100 m away from both northern indaries of the desalination plant as shown in

No.	Parameters	Design Requirements / Measures in 2017 ERR	Recommendations in 2021 DDP	Audit Results - A
5.10	Separation distance between CO2 storage area and toe of natural slope behind	Approximately 30m	Approximately 30m for CO ₂ storage in DP1	The as-built CO ₂ 2021 DDP. It is si indicated in App
5.11	Safety measure to protect the CO ₂ storage area from soil debris.	A 1.5m high baffle barrier will be constructed at the roadside of the internal access road.	No change to the safety measure is proposed.	A 1.5 m high barn record in Appen

2 storage area in DP1 follows the recommendations in situated at more than 30 m away from the slope toe in pendix B-13 and Appendix C.

rrier has been provided as indicated in the photo **ndix B-14**.

3 Conclusion

3.1.1 An audit has been carried out in accordance with Condition 2.20 of FEP No. FEP-01/503/2015/A and EP No. EP-01/503/2015/A for certifying the implementation of design requirements / measures recommended in the 2021 DDP approved under Condition 2.12 of the FEP and EP. The audit results showed that the design requirements and measures for mitigating hazard to life as recommended in the 2021 DDP have been implemented at DP1. With the provision of these design requirements and measures, operation of the DP1 would not induce additional hazard to life impact as compared to the predictions in the 2017 ERR and 2021 DDP.

End of Text

Appendix A Design Requirements and Measures for OSCG, Chemical Handling and Storage



DATE:









Appendix A-3 OSCG Design Data Sheet

First Stag	ge of Tseun	g Kwan O Des	alination Plant	:	
Rev:	6		ETS CH	ILORINATION SI	ZE JUSTIFICATION
Created By:	E.P.		DESIGN SCENARIOS		
OSCG PRODU	ICTION SKID				
	Care	Stage 1	Store 1	Stage 1	
	Case	25% Guaranteed	100% Guaranteed	Annual	-
		25%	100%	106%	-
Duty Units		1	1	1	_
Stand-By Units	Deaduction	1	1	1	(hald
Minimum Turn	down Ratio	16%	213	213	KB/0
In the second second	down Natio	Note: Below 20% turn	down_energy_consumpt	ion on OSCG will I	he higher the guarantee performance
Flow		35.674	135.000	142,694	m3/d
Cl2 Dose Minim	num	1.0	1.00	1.00	ppm
NaOCI Back Up	(as Cl2)	0	0	0	
Cl2 Production		35,67	135,00	142,69	kg/d
NaOCI Back Up	(as CI2)	0,00	0,00	0,00	kg/d
Frequency		Continuous	Continuous	Continuous	
Total Postreate	ement	35,67	135,00	142,69	kg/d
					7
Intake Flow		84.795	339.178	354.952	m3/d
CI2 Dose		0.00	0	0	ppm ka/shask
Ciz Production		14	14	0,00	davr.
Total Intake		0.00	0.00	0.00	ka/d
Total intake		0,00	0,00	0,00	ng u
Total		35,67	135,00	142,69	kg/d
Turndown		16,7%	63,4%	67,0%	
					-
CI2 Dose Status	5	ОК	OK	ОК	0.5 <dose<1.5< td=""></dose<1.5<>
TD Status		ОК	ОК	ОК	16% <td<100%< td=""></td<100%<>
OSCG NaOCI	TANKS				
Average Dose		1	1	1	ppm
Storage time		20,00	20,00	20,00	days
NaOCI Concent	tration	6,00%	6,00%	6,00%	
Volume Storner		10.91	1100	1100	kg/m3
Volume storage	e	10,81	40,91	45,24	
Tanks at OSCG	Building	3	3	3	
Tank Capacity		17	17	17	m3
Storage Days a	t OSCG B	94,36	24,93	23,59	days
Total Storage C	apacity	94,36	24,93	23,59	days
Storage Capaci	ty Status	OK	ОК	ОК	Storage>20 days

Appendix A-4 Data Sheet of OSCG Ventilation Fans (Sheet 1 of 3)

	Floor Level	Room Dimension			Environme Conc	ental Design dition	esign		Occupants		Outdoor Air					
Room Name		Floor Area	Height	Volume	System	Design Temperature	Humidity	Equipment Load	Lighting Load	Default Occupant Density	No. of Occupants	Metabolic Heat	People Outdoor Air Rate	Area Outdoor Air Rate	Combined Outdoor Air rate	Outdoor Air Rate
		m²	m	m³	AC/MV/NV	°C	%	kW	W/m ²	m²/pr	pr	W/pr	L/s/pr	L/s/m ²	L/s/pr	L/s
Scrubber	GF	15.2	6.6	100	ž	40	Uncontrolled	0	10		2	450	•	•		
Electrical Room	GF	74.8	6.6	494	AC	28	Uncontrolled			-			•	-		
Big Bag Salt Storage	GF	128.5	6.6	<mark>848</mark>	MV		50									
Chlorinators Room	GF	11.4	6.6	75	MV	40	Uncontrolled	0.85	10	-	2	450	•	-		
Electrolyser and Rectifier Room	GF	247.3	6.6	<mark>1632</mark>	Ň	40	Uncontrolled	0.7	10		2	450		-		
Sodium Hypochlorite Tank Store (Cat No.4)	GF	57.5	6.6	<mark>380</mark>	MV		-			-				-		
Filtered Brine Tank Room	GF	38.1	6.6	251	MV											
Equali Tank and Neutra Tank Room	GF	35.0	5.3	186	MV	40	Uncontrolled	0.5	10		2	450	-			

| Water Supplies Department

Appendix A-4 Data Sheet of OSCG Ventilation Fans (Sheet 2 of 3)

			ACH Method				Heat Gain Method			Heat Ga	in Method					
Room Name	Floor	Outdoor	% of	Exhaust Air by	Exhaust Air		Exhaust Air		Solar Heat	Gain		Solar H	leat Gain		Plant H	leat Gain
	Level	Air in ACH Extract Air	Extract Air	heat load	by Area	ACH	Exhaust Air	Solar Vertical	Intensity Horizonatal	Material	Transmission	A Vertical	rea Horizonatal	Solar Heat Load	Lighting Load	Electrical Load
		ACH	%	/	L/s/m2		L/s	kW/m ²	kW/m ²		factor	m²	m²	kW	kW	kW
Scrubber	GF	-	100		-	6	167	0.71	1.03	250mm concrete	0.08	31	15	3.03	0.15	0.0
Electrical Room	GF	-		-				1	-	-			-			-
Big Bag Salt Storage	GF		100			6	1464									
Chlorinators Room	GF					6	125	0.71	1.03	250mm concrete	0.08	30.5	11	2.67	0.11	0.9
Electrolyser and Rectifier Room	GF	-	100		-	6	2753	0.71	1.03	250mm concrete	0.08	130	247	27.76	2.47	0.7
Sodium Hypochlorite Tank Store (Cat No.4)	GF	-	100			6	<mark>633</mark>									
Filtered Brine Tank Room	GF	-	100	-		6	419		-	-	-		-	-	-	-
Equali Tank and Neutra Tank Room	GF		100			6	309	0.71	1.03	250mm concrete	0.08	22	35	4.13	0.35	0.5

| Water Supplies Department

Appendix A-4 Data Sheet of OSCG Ventilation Fans (Sheet 3 of 3)

	Floor Level	Heat Gain Meth	od		ACH Method	Exhaust Air Flow Rate			
Room Name		Metabolic Heat Gain People Load (0.45kW per person)	Total Heat Gain	Temperature Rise	Exhaust Air	Exhaust Air	Required (Compared ACH & Heat Gain Method)	Total Exhaust Air Flow Rate Provided	
		kW	kW	°c	L/s	L/s	L/s	L/s	
Scrubber	GF	0.9	4.09	5	692	<mark>167</mark>	692	700	
Electrical Room	GF	-	-	-	-	-	-	-	
Big Bag Salt Storage	GF	-	-	-	-	<mark>1464</mark>	1464	1470	
Chlorinators Room	GF	0.9	4.54	5	769	<mark>125</mark>	769	770	
Electrolyser and Rectifier Room	GF	0.9	31.84	5	5396	2753	5396	<mark>5400</mark>	
Sodium Hypochlorite Tank Store (Cat No.4)	GF					<mark>633</mark>	633	<mark>640</mark>	
Filtered Brine Tank Room	GF		-	-		<mark>419</mark>	419	420	
Equali Tank and Neutra Tank Room	GF	0.9	5.88	5	997	<mark>309</mark>	997	1000	



)[
				22 550 2022
BI	DETAILED DESIGN APPROVAL		WYF	23 DEC 2022
BO	DETAILED DESIGN APPROVAL		WYF	07 MAY 2021
A0	APPROVAL IN PRINCIPLI	E	WYF	31 JUL 2020
Rev	Description		Ву	Date
Supe	IN Checker	er Supplies	s Dep CS	sign & Consultancy matural and ilt assets
Contr	actor		EC CJU	RE
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Proje	ct title		In As	sociation with APU
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	SIGN, BUILD AND C)PERATE UNG KWAN C)	
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THIS DRAWING IS GENERATED FROM REVIT MODEL

Appendix A-6 OSCG Building Volume



GBP-EVA DIAGRAM

NOTES OF EVA:

1:200

- 1. THE DESIGN OF THE FORMATION EVA SHALL BE CAPABLE OF RESISTING THE WEIGHT OF THE FIRE APPLIANCE 30,000kg.
- 2. ANY OVERHEAD STRUCTURE OVER ABOVE EVA, A CLEAR HEADROOM SHOULD BE MAINTAINED WITH A MIN. 4.5 METERS THROUGHOUT THE EVA ROUTING.
- 3. NO PART OF THE GRADIENT THROUGHOUT THIS ACCESS ROAD IF STEEPER THAN 1 IN 10
- 4. NO PART OF THE WIDTH THROUGHOUT THIS EVA IS LESS THAN 7.3 METERS WIDE OR OTHERWISE SPECIFIED.
- 5. THE EVA SHALL BE HARD PAVED.
- 6. AN EVA LAYOUT SIGN SHALL BE ERECTED AT THE ENTRANCE OF THE SITE.
- 7. EVA EMERGENCY ROUTE SIGNS SHALL BE POSITIONED AT AN INTERVAL OF NOT LESS THAN 100M ALONG THE EVA.
- 8. NO PARKING SIGNS SHALL BE ERECTED ALONG THE EVA AT 50M INTERVALS EXCEPT WHERE DISGNATED CARPARKS ARE MARKED.



TOTAL LENGTH OF ALL PERIMETER WALL (OSCG)

SEGMENT MARK	LENGTH OF PERIMETER WALL
R2	46.912 m
R3	4.206 m
R4	<u>1.200 m</u>
R5	14.329 m
R6	1.195 m
R7	32.583 m
RA	12.439 m
RB	16.650 m
Grand total	129.514 m

LENGTH OF FACADE TO BE SERVED BY EV							
SEGMENT MARK	LENGTH OF PERIMETER WALL						
R2	46.912 m						
R3	4.206 m						
R4	<u>1.200 m</u>						
R5	14.329 m						
R6	1.195 m						
R7	32.583 m						
Grand total	<u>100.425 m</u>						

			PROVISION OF	EXIT DOO	RS & EXII	ROUIESF	ROMSTO	KEY				
				OCCUPANCY	OCCUPANT	MIN. NOS. OF EXIT DOOR & EXIT ROUTE	MINIMUM TOTAL WIDTH (IN MM)			MINIMUM W		
							EXIT DOORS EXIT ROUTES		OUTES	EXIT DOOR		
LEVEL	NAME	Area	USE CLASSIFICATION	FACTOR	CAPACITY	PROVIDED	REQUIRED	PROVIDED	REQUIRED	PROVIDED	REQUIRED	PROVIDE
GROUND FLOOR	BIG BAG SALT STORE ROOM	125.672 m ²	PLANT ROOMS (>100M2)	30	5	2		900		1050	750	900
GROUND FLOOR	DG STORE 1 CLASS 8 (SODIUM BISULPHITE)	<u>17.602 m²</u>	STORAGE , MANUFACTURING OF HAZARDOUS / DANGEROUS GOODS PREMISES	30	1	1		900		1050	750	900
GROUND FLOOR	DG STORE 2 CLASS 8 (HYDROCHLORIC ACID)	<u>37.183 m²</u>	STORAGE , MANUFACTURING OF HAZARDOUS / DANGEROUS GOODS PREMISES	30	2	1		900 🔺	* = :	1050	750	900
GROUND FLOOR	DG STORE 3 CLASS 8 (SODIUM HYDROXIDE)	<u>37.190 m²</u>	STORAGE , MANUFACTURING OF HAZARDOUS / DANGEROUS GOODS PREMISES	30	2	1		900		1050	750	900
GROUND FLOOR	DG STORE 4 CLASS 8 (SODIUM HYPOCHLORITE)	57.436 m ²	STORAGE , MANUFACTURING OF HAZARDOUS / DANGEROUS GOODS PREMISES	30	2	1		900		1050	750	900
GROUND FLOOR	ELECTROLYSER SKID STREAM ROOM	250.516 m ²	PLANT ROOMS (>100M2)	30	9	2		3400		1050	750	900







DATE





Appendix A-8 Ventilation System and Scrubber Operation Philosophy (Sheet 1 of 2)



Contract No. 13/WSD/17 Design, Build and Operate First Stage of Tseung Kwan O Desalination Plant



OSCG PLANT

VENTILATION SYSTEM AND SCRUBBER OPERATION PHILOSOPHY

1. VENTILATION SYSTEM

The ventilation system at the "Electrolyzers Skid Stream Room" and "Chlorinators Room" comprises of:

- a. High level air intake wall louvers, equipped with motorized dampers
- b. Ventilation fans, are provided with extraction air ducts for low level extraction
- c. High level air extraction wall louvers, equipped with motorized dampers, for air exhaust via the ventilation fans.

2. DRY CHLORINE SCRUBBER SYSTEM

One dry type chlorine scrubber is provided at the "Scrubber Room". Low level extraction air ducts are provided around the skid areas to ensure effective extraction of chlorine to the scrubber for adsorption via the scrubber fans.

3. AMBIENT CHLORINE GAS DETECTORS

Seven (7) nos. ambient chlorine gas detectors will be located at low levels inside the "Electrolyzers Skid Stream Room" to detect the ambient chlorine level.

One (1) no. ambient chlorine gas detector will be located at low levels inside the "Chlorinator Room" to detect the ambient chlorine level.

Please refer to drawing TKOD1-DWG-R001-WFS1011 showing the locations of above detectors.

All the chlorine detectors are default at <u>1 ppm</u> for low leakage alarm and <u>3 ppm</u> for high leakage alarm. Manual Call Point will be treated as high leakage alarm at the detection area. Please see below Part 5 for the alarm and control logic of chlorine gas detection. Visual and audio alarms in Electroyzers Skid Stream Room" and "Chlorinator Rooms shall be activated. The siren and amber light at the gas detection local panel shall be maintained.

4. SCRUBBER CONTROL

On detection of chlorine leak within "Electrolyzers Skid Stream Room" or "Chlorinator Room" at and above <u>3 ppm</u>, or initiated by a manual activation call point, the OSCG plant will shut down and the plant room normal ventilation system will stop with all motorized wall louvres and dampers closed.

The scrubbers will start to extract the air inside the above two rooms via the low level ducts to the dry chlorine scrubber. The dry chlorine scrubber is designed with 99.5% removal efficiency of media absorption. The scrubbed air will be allowed to discharge back to the above rooms. Three detectors to give triple validation are located at the scrubber discharge to monitor the chlorine level of scrubbed air.

Appendix A-8 Ventilation System and Scrubber Operation Philosophy (Sheet 2 of 2)



Contract No. 13/WSD/17 Design, Build and Operate First Stage of Tseung Kwan O Desalination Plant



The stopped of the scrubber will only be initiated manually by the operator.

5. CHLORINE LEAKAGE ALARM AT ELECTROLYZERS SKID STREAM ROOM, SCRUBBER ROOM AND CHLORINATOR ROOM

Low Leakage alarm - Chlorine gas detection at <u>1 ppm</u> or above (low leakage alarm):

- The Gas Detection Control Panel triggers and latches the siren and amber light at the gas detection local panel;
- (2) The Gas Detection Control Panel activates the Emergency Shutdown Device (ESD);
- (3) The ESD sends the low chlorine gas leakage alarm signal through the distributed control system;

High Leakage alarm - Chlorine gas detection at 3 ppm or above (high leakage alarm):

- The Gas Detection Control Panel triggers and latches the siren and amber light at the gas detection local panel;
- (2) The Gas Detection Control Panel sends an alarm signal through OSCG sub-main AFA system to main AFA panel in guard house A;
- (3) The Gas Detection Control Panel activates the ESD
- (4) The ESD activates the scrubber system (scrubber control panel) (please see above Part 4 for the scrubber control for detail);
- (5) The ESD shuts down OSCG 1 and OSCG 2 (motor control panel);
- (6) The ESD shuts down the ventilation fans of chlorine gas detector areas (ventilation fan control panels in "Chlorinator Room" and "Electrolyzers Skid Stream Room")
- The ESD shuts down the motorised dampers of chlorine gas detector areas (damper control panel);
- (8) The ESD sends the high chlorine gas leakage alarm signal through the distributed control system.

6. HYDROGEN GAS DETECTION ABOVE 1% SETPOINT VALUE (HYDROGEN LEAKAGE ALARM)

- (1) The Gas Detection Control Panel triggers and latches the siren and amber light at the gas detection local panel;
- (2) The Gas Detection Control Panel sends an alarm signal through OSCG sub-main AFA system to main AFA panel in guard house A.
- (3) The Gas Detection Control Panel activates the ESD
- (4) ESD sends signals to Hydrogen Exhaust Fan Control Panel to activate the hydrogen extraction ventilation fans;
- (5) ESD shuts down OSCG 1 and OSCG 2 plants through the motor control panel;
- (6) The ESD sends the hydrogen gas leakage alarm signal through the distributed control system

Appendix A-9 Chorine Detector Coverage

NOTES:

- PRESET VALUES OF CHLORINE DETECTION LEVELS ARE 3PPM AND 1PPM FOR 'HIGH CHLORINE LEAK' AND 'LOW CHLORINE LEAK' RESPECTIVELY. UPON RECEIVING A LOW CHLORINE LEAKAGE ALARM FROM A GAS DETECTOR, THE SIREN AND AMBER LIGHT AT THE GAS DETECTION LOCAL PANEL SHALL BE TRIGGERED AND LATCHED. VISUAL & AUDIO ALARMS IN HAZARDOUS AREA SHALL BE ACTIVATED
- UPON RECEIVING A HIGH CHLORINE LEAKAGE ALARM, THE SIREN AND AMBER LIGHT AT THE GAS DETECTION LOCAL PANEL SHALL 2. BE MAINTAINED. VISUAL & AUDIO ALARMS IN HAZARDOUS AREA SHALL BE MAINTAINED. THE VENTILATION FANS SERVING THAT AREA WILL BE SHUT DOWN AND THE DAMPERS AT THE VENTILATION DUCT AND INTAKE LOUVRE WILL BE CLOSED. THE CHLORINE SCRUBBER SYSTEM WILL BE OPERATED, AND THE SIREN AND AMBER LIGHT AT THE GAS DETECTION LOCAL PANEL SHALL BE TRIGGERED AND LATCHED.
- UPON DETECTION OF HYDROGEN GAS LEAKAGE ABOVE 1% BY VOLUME, HYDROGEN EXTRACTION VENTILATION FANS SHALL START AUTOMATICALLY AND THE OSCG PLANTS SHALL BE AUTOMATICALLY SHUT DOWN ACCORDING TO THE PRE-SET HYDROGEN CONCENTRATIONS. THE SIREN AND AMBER LIGHT AT THE GAS DETECTION LOCAL PANEL SHALL BE TRIGGERED AND 3. LATCHED.VISUAL & AUDIO ALARMS IN HAZARDOUS AREA SHALL BE ACTIVATED.
- 4. ALL GAS DETECTORS SHALL BE INTRINSICALLY SAFE DETECTORS. ALL HEAT DETECTORS IN SCRUBBER ROOM, CHLORINATORS ROOM AND ELECTROLYSER SKID STREAM ROOM SHALL BE EXPLOSION PROOF
- 5. THE MOTORS OF THE VENTILATION FANS IN ELECTROLYSER SKID STREAM ROOM IN SHALL BE NON-SPARKING TYPE.
- 6. DOUBLE BEND LOUVER WILL BE USED.
- 7. DOUBLE CONTAINMENT WILL BE USED FOR HYDROCHLORIC ACID PIPES.
- 8. DETAILS OF THE DG STORE ROOMS 1 TO 4 ARE SHOWN IN SEPARATE SUBMISSION FOR APPLICATION FOR LICENSE FOR STORAGE OF DANGEROUS GOODS
- 9. THE MECHANICAL VENTILATION SYSTEMS SHOULD COMPLY WITH THE REQUIREMENTS OF FSD CIRCULAR LETTER NO. 4/96 PART XI AND THE BUILDING (VENTILATING SYSTEMS) REGULATIONS CAP. 123J, WHICHEVER APPLICABLE.
- 10. LOUVERS SHOWN IN THIS SUBMISSION ARE FOR NATURAL / MECHANICAL VENTILATION ONLY, EXCESSIVE ARCHITECTURAL FEATURE LOUVERS WILL BE BLANKED OFF.
- 11. FOR DETAILS OF THE EQUIPMENT INSIDE THE ELECTROLYSER SKID STREAM ROOM, SCRUBBER ROOM AND CHLORINATORS ROOM, REFER TO TKOD1-DWG-R001-AFS0001 AND AFS0002.









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Appendix A-10 Process & Instrumentation Diagrams (P&IDs) of Scrubber



| Water Supplies Department

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	1"	DN25	12"	DN30	0		
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	2 1/2"	DN65	18"	DN45	0		
	3"	DN80	20"	DN50	0		
	4″ 5″	DN100 DN125	24"	DN60 DN70	0		
	6"	DN150	32"	DN80	0		
B2 B1 B0 Rev	B3 DDA SUBMISSION B.A. 03/23 B2 DDA SUBMISSION B.A. 11/22 B1 DDA SUBMISSION M.P. 06/21 B0 DDA SUBMISSION M.P. 05/21 Rev Description By Date						
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Contr	Contractor Contractor AJC JOINT VENTURE Designer						
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Drawin TK(Drawin B.A. Scole	Drowing no. B3 TKOD1-PID-R001-APE0050 B3 Drown Date Approved JA. JA. JA. Scale % Stotus ©COPYRIGHT RESERVED						

Appendix A-11 "No Objection" Reply from EPD on the Submission of Dry Type Scrubber for the OSCG (Sheet 1 of 4)

Binnies-April Wong <ca></ca>		190495/(13/WSD/17)/M45/100/M201348		
收件者: 副本: 主旨:	Binnies-Phoebe Ho <co> Binnies-Fannie Fong<aco RE: 13/WSD/17 - AJC/EPD/ Chlorine Generation Plant</aco </co>	>; Binnies-Vivi Chan <aco>; Binnies-Eli Hui<aco> (230012 Submission of Dry Type Chlorine Scrubber for the On-Site (OSCG)</aco></aco>		
From: Binnies	-Anthony Mok <sre.m&e> <<u>sre4</u></sre.m&e>	@bv13wsd17.com.hk>		

Sent: Monday, June 12, 2023 5:56 PM

To: WSD-LAW Wai Ho, Milton<Sr Engr/CM2> <<u>wh_law@wsd.gov.hk</u>>; WSD-LAI Hon Lam, Jack<Engr/CM5> <<u>jack_hl_lai@wsd.gov.hk</u>>; Binnies-Phoebe Ho<CO> <<u>co@bv13wsd17.com.hk</u>> Cc: BinniesHK-Christina KO<Senior Project Manager> <<u>kosc@binnies.com</u>>; Binnies-Roger Wu<CRE>

<<u>cre@bv13wsd17.com.hk</u>>; JEC-Stephen Yeung<Project Manager> <<u>stephen.cw.yeung@jec.com</u>>; ACC-Sergio Pinelo Otero<Project Manager> <<u>spinuelo@acciona.com</u>>; Binnies-Aldous Lee<RE.Mech.>

<re11@bv13wsd17.com.hk>; Binnies-Patrick MAK<RE.Mech.> <re10@bv13wsd17.com.hk>

Subject: FW: 13/WSD/17 - AJC/EPD/230012 Submission of Dry Type Chlorine Scrubber for the On-Site Chlorine Generation Plant (OSCG)

Dear all,

<u>RE: AJC/EPD/230012 Submission of Dry Type Chlorine Scrubber for the On-Site Chlorine</u> Generation Plant (OSCG)

For you information and record, attached is the email from EPD stating no comment on the Submission of Dry Type Chlorine Scrubber for the OSCG Plant. This email <u>serves as formal</u> <u>reply of no objection to the proposed installation</u>. Meanwhile the only outstanding issue is the submission for manufacturing license for OSCG system, which will be re-submission this week.

Dear Phoebe,

Please record this email under EDMS file M45/100.

Best regards, Anthony MOK Tel: 9155-8863

From: kyng@epd.gov.hk <kyng@epd.gov.hk>

Sent: Monday, June 12, 2023 5:09 PM

To: 甘忠校 < chunghau kam@cohl.com>

Cc: Billy Chan < billy.chan@iec.com >; Bidaurrazaga Marijuan, Jose Andres

<joseandres.bidaurrazaga.marijuan@acciona.com>; CSHK-Chung Kam Fai, Jason<施工經理>

<<u>kamfai_chung@cohl.com</u>>; Binnies-Aldous Lee<RE.Mech.> <<u>re11@bv13wsd17.com.hk</u>>; ACC-Sergio Pinelo Otero<Project Manager> <<u>spinuelo@acciona.com</u>>; Binnies-Anthony Mok<SRE.M&E> <<u>sre4@bv13wsd17.com.hk</u>>; JEC-Stephen Yeung<Project Manager> <<u>stephen.cw.veung@iec.com</u>>; CSHK-Laurence Wong<Project Manager> <<u>wingkeung_wong@cohl.com</u>>

Subject: RE: 13/WSD/17 - AJC/EPD/230012 Submission of Dry Type Chlorine Scrubber for the On-Site Chlorine Generation Plant (OSCG)

Appendix A-11 "No Objection" Reply from EPD on the Submission of Dry Type Scrubber for the OSCG (Sheet 2 of 4)

Dear Brian,

My email reply to you dated 10:28 today serves as a formal reply of no objection to the proposed installation. Thank you!

Regards, Jacky Ng E(ASM)82 Tel: 2835 2142

 From:
 甘忠枝 <<u>chunghau_kam@cohl.com</u>>

 To:
 "kyng@epd.gov.hk" <<u>kyng@epd.gov.hk</u>"

 C::
 Billy Chan <<u>billy_chan@lec.com</u>>, "Bidaurrazaga Marijuan, Jose Andres" <<u>joseandres.bidaurrazaga.marijuan@acciona.com</u>>, #ißi#i

 Kamfai_chung@cohl.com>, "BV-Aldous Lee<RE.Mech.>" <<u>req11@bv13wsd17.com.hk</u>>, "ACC-Sergio Pinelo Otero<Project Manager>"<<u>solnuelo@acciona.com</u>>, "Binnles-Anthony Mok<SRE.M&E>" <<u>sreq4@bv13wsd17.com.hk</u>>, "JEC-Stephen Yeung<Project Manager>"<<u>solnuelo@acciona.com</u>>, "Wong, Wing Keung (CN - Hong Kong)" <<u>wingkeung_wong@cohl.com</u>>

 Date:
 12/06/2023 16:59

 Subject:
 RE: 13WSD/17 - AJC/EPD/230012 Submission of Dry Type Chlorine Scrubber for the On-Site Chlorine Generation Plant (OSCG)

Dear Jacky,

Thanks for your time and vetting. To address our Employer's and the Supervising Officer's concern, we would like to check if the below message would serve as a formal reply of no objection to our proposed scrubber installation.

Best Regards, Brian Kam

Env Monitoring Mgr Mobile (852-9456 9541) Design, Build and Operate First Stage of Tseung Kwan O Desalination Plant AJC Joint Venture

From: kyng@epd.gov.hk <kyng@epd.gov.hk> Sent: Monday, June 12, 2023 10:28 AM

To:甘忠校 <<u>chunghau kam@cohl.com</u>>

Cc: Billy Chan < billy.chan@jec.com; #); #); <a href="https

錦輝 <<u>kamfai_chung@cohl.com</u>>; BV-Aldous Lee<RE.Mech.> <<u>re11@bv13wsd17.com.hk</u>>; ACC-Sergio Pinelo Otero<Project Manager> <<u>spinuelo@acciona.com</u>>; Binnies-Anthony Mok<SRE.M&E> <<u>sre4@bv13wsd17.com.hk</u>>; JEC-Stephen Yeung<Project Manager> <<u>stephen.cw.yeung@iec.com</u>>; Wong, Wing Keung (CN - Hong Kong) <<u>wingkeung_wong@cohl.com</u>> **Subject:** RE: 13/WSD/17 - AJC/EPD/230012 Submission of Dry Type Chlorine Scrubber for the On-Site Chlorine Generation Plant (OSCG)

Dear Brian,

I refer to your preceding emails for the subject matter. Based on the information provided, the proposed dry type chlorine scrubber for the OSCG Plant has chlorine removal efficiency of

Appendix A-11 "No Objection" Reply from EPD on the Submission of Dry Type Scrubber for the OSCG (Sheet 3 of 4)

higher than 99.99% and availability of higher than 99%. Therefore, please be advised that we have no comment on the proposed installation from non-fuel gas dangerous goods risk perspective.

Regards, Jacky Ng, E[ASM]82

Dear Jacky,

May I coordinate our response (w/ reference to the page of submission document) to your queries as below.

1. Confirmation of removal efficiency of the scrubber system be >99%

Its minimum removal efficiency of Purafil system is 99.5% as shown in the product catalogue (page 8 -16 o the submission document). Further, the calculation of absorber performance and removal efficiency has been provided in page 125 to 127 (Section E) of the submission document.

Application Guidelines

-40°F to 125°F (-40°C to 51°C)
10 - 95% RH
60 - 500 fpm (0.30 - 2.54 m/s)
99.5% (min)initial removal efficiency in Purafil systems

2. Availability of the scrubber system >99% ?

The availability is about 99.18% where its calculation has been provided in page 124 (Section D) of the submission document.

3. One scrubber or more installed ?

One scrubber and two blowers installed. The information has been provided in page 6 (Section A data sheet) and page 141 (para 2 of Section F) of the submission document.

Please let us know should you have any further query. Thanks for your attention and assistance.

Regards,

Brian

From: 甘忠校

Sent: Friday, June 9, 2023 11:23 AM

To: 'kyng@epd.gov.hk' <<u>kyng@epd.gov.hk</u>>; 'Billy Chan' <<u>billy.chan@jec.com</u>>

Cc: 'JEC-Stephen Yeung<Project Manager>' <<u>stephen.cw.yeung@jec.com</u>>; 'ACC-Sergio Pinelo Otero<Project Manager>' <<u>spinuelo@acciona.com</u>>; 'Binnies-Anthony Mok<SRE.M&E>' <<u>sre4@bv13wsd17.com.hk</u>>; 'BV-Aldous Lee<RE.Mech.>' <<u>re11@bv13wsd17.com.hk</u>>; Wong, Wing Keung (CN - Hong Kong) <<u>wingkeung_wong@cohl.com</u>>; 鍾錦輝
Appendix A-11 "No Objection" Reply from EPD on the Submission of Dry Type Scrubber for the OSCG (Sheet 4 of 4)

<<u>kamfai_chung@cohl.com</u>>

Subject: FW: 13/WSD/17 - AJC/EPD/230012 Submission of Dry Type Chlorine Scrubber for the On-Site Chlorine Generation Plant (OSCG)

Dear Jacky,

Thanks for your call this morning. Attached please find the softcopy as requested. For your other enquires below, may I direct to our respective team member to respond/ reply.

- 1. Confirmation of removal efficiency of the scrubber system be >99%
- 2. Availability of the scrubber system >99% ?
- 3. One scrubber or more installed ?

By copy to Billy, would you help respond the above by citing the respective section in the submission document, please.

Best Regards, Brian Kam

Env Monitoring Mgr Mobile (852-9456 9541) Design, Build and Operate First Stage of Tseung Kwan O Desalination Plant AJC Joint Venture

Appendix A-12 BIM Screen Shot of OSCG and Chemical Building



Appendix A-13 Supporting Information on Hydrogen Gas Dilution



L	EGE	ND		
_	L	- AFA ADDRESSABLE LOOP CIRCU	IT	
	P	- 24V DC POWER SUPPLY CIRCUIT	ſ	
_		- TWISTED PAIR CABLE		
		- CONTROL CABLE		
C	ESD	EMERGENCY SHUTDOWN SYSTEM CHLORINE GENERATION PLANTS	OF ON	-SITE
Ĥ	(ASH	FLASHING LIGHT		
	Ð	HEAT DETECTOR		
	© ⁰²	CHLORINE GAS DETECTOR		
(© ^{CI2 EX}	CHLORINE GAS DETECTOR (EXPL	DSION F	PROOF)
(© ^{H2}	HYDROGEN GAS DETECTOR (EXPL	OSION	PROOF)
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[BREAK GLASS UNIT FOR CHLORI	NE DETI 71.	ECTION
	ŏ	ALARM BELL 비생	ľ	IN-LINE AXIAL FAN
	C	FS CONTROL MODULE		
_	M	FS MONITOR MODULE		
[9 \$	CENTRIFUGAL FAN		
	1	MOTORISED DAMPER		
ŀ	ABB	REVIATION		
I	EXF	EXHAUST FAN		
	OSCG	ON-SITE CHLORINE GENERATION	SYSTE	М
NI/	MD () TF	MOTORISED DAMPER		
1				CVCTEM CHALL
1.	HAVE	A MINIMUM OF TWO (2) SPARE	ZONES	IN THE ALARM
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Appendix A-14 Extract from OSCG Material Submission (Hydrogen Dilution)



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Appendix A-15 BIM Model Separation Distances Between Facilities in OSCG



Audit Report on Measures for Mitigating Hazard to Life

Appendix A-16 P&ID Showing Tanker Filling Point and Control Valve for Ferric Chloride Storage in Chemical Building

	EQUIVALE	N	CE TABLE		
IOMINAL PE SIZE NPS INCHES	NOMINAL DIAMETER DN mm		NOMINAL PIPE SIZE NPS INCHES	NOMINAL DIAMETER DN mm	
3/8"	DN10		8"	DN200	
1/2"	DN15		10"	DN250	
1"	DN25		12"	DN300	
1 1/2"	DN40		14"	DN350	
2"	DN50		16"	DN400	
2 1/2"	DN65		18"	DN450	
3"	DN80		20"	DN500	
4"	DN100		24"	DN600	
5"	DN125		28"	DN700	
6"	DN150		32"	DN800	

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DA SUBMISSION	A.P.	03/22
DA SUBMISSION	A.P.	06/21
DA SUBMISSION	B.A.	02/21
DA SUBMISSION	C.C.	11/20
OR REVIEW	A.L.R.	06/20
OR REVIEW	C.C.	03/20
Description	By	Date

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Appendix A-17 P&ID Showing Tanker Filling Point and Control Valve for Sodium Hypochlorite Storage in Chemical Building

T1GAC16BB001//002	T1GAC16AP001//003		
SODIUM HYPOCHLORITE STORAGE TANK	SODIUM HYPOCHLORITE INTAKE DOSING PUMP		
USEFUL VOLUME: 8.5 m3.	FLOW: 3,410.47 l/h.		
MATERIAL: GRP	PRESSURE: 3 bar		
	POWER: 4 kW		
.UNITS:2	.UNITS: 1 DUTY , 1 STANDBY		







Audit Report on Measures for Mitigating Hazard to Life

Appendix A-18 P&ID Showing Tanker Filling Point and Control Valve for Sulphuric Acid Storage in Chemical Building

| Water Supplies Department







| Water Supplies Department

	NOTES: 	
	EQUIPMENT SIZING - CHEMICALS FOR FURTHER	INFORMATION
	-CHEMICAL DIAPHRAGM SEALS WILL BE INCLUDED	IN THE PRESSURE
	INSTRUMENTATION IF THE MATERIALS ARE NOT C CHEMICAL.	COMPATIBLE WITH THE
	-CHECK VALVES FOR DISCHARGE PIPES ARE INTE DOSING PLIMPS	GRATED IN THE
	-EQUIPMENT POWER VALUES ARE INDICATIVE AND	WILL BE CONFIRMED
	-COMMERCIAL PROUDUCT CONCENTRATION: 13% /	AS FREE CHLORINE.
	TKOD1 – DWG-A000 – WGN000 10002;0003;0004;01	005;0006
	-NOTE 1: CROSSEINCED PE WITH ANTIONIDATION -NOTE 2: HANDHOLE FOR TANK FLUSHING	DARRIER
	-NOTE 4: VENTED BALL VALVES TO BE USED.	DESIGN
	RESPONSABILITY INCLUDE ELEMENTS INSIDE THE	MARKED AREA.
	INCLUDING PIPE DIAMETER AND FLOWS. PIPE ARRANGEMENTS, SUPPORTS AND CIVIL DESIG	SN ARE OUTSIDE
	ELECTROLYTIC TECHNOLOGIES SCOPE	
	TECHNOLOGIES AND CONNECTED TO ELECTROLYTIC	C TECHNOLOGIES PLC'S
	(LOCAL INDICATION INSTRUMENTS JUST SUPPLIED) -NOTE 7: FLEMENTS MARKED WITH (**) ARE SUIT	PPLIED BY
N	ELECTROLYTIC TECHNOLOGIES AND CONNECTED TO	ACCIONA DCS.
	TANK BOTTOM.	E FLUSHED WITH THE
	Electrolytic	
i	rechnologies	
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	PIPE SIZE DIAMETER PIPE SIZE	DIAMETER
i	INCHES MM INCHES	DN
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) !	1/2" DN15 10"	DN250
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	Drawing title	
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!	SODIUM HYPOCHLORITE	STORAGE
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	Drawing no.	Rev.
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Appendix A-20 P&ID Showing Tanker Filling Point and Control Valve for Hydrochloric Acid Storage in OSCG Building



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Appendix A-21 P&ID Showing Tanker Filling Point and Control Valve for Sodium Bisulphite Storage in OSCG Building

0 0		 		
T1GCM48BB001.		T1GCM48AP001//002	T1GCM48AP003//004	
SODIUM BISULPHITE STORAGE TANK		DOSING PUMP	DOSING PUMP	
CAPACITY: 1.8 m3.		FLOW: 90 l/h.	FLOW: 90 I/h.	
MATERIAL: XLPE		PRESSURE: 6 bar	PRESSURE: 6 bar	
NOTE 1				
.UNITS:2		.UNITS:1 DUTY , 1 STANDBY	.UNITS:1 DUTY , 1 STANDBY	



	-REFER EQUIP	<u>S:</u> TO TKOD1-CA MENT SIZING-C	L-R001-APE00 HEMICALS FOR	01 PROCESS OF FURTHER INFOR	CALCULATION	S &
	PROCE -PROUD -CHEMIC	SS PARAMETER UCT PREPARAT CAL DIAPHRAGN	S. ION CONCENTR I SEALS WILL E	ATION: 22.5% S IE INCLUDED IN	ODIUM BISU	LPHITE. SURE
	INSTRU CHEMIC -CHECK	IMENTATION IF CAL, VALVES FOR	THE MATERIALS DISCHARGE PIP	ARE NOT COM ES ARE INTEGR	IPATIBLE WIT ATED IN THI	h the E dosing
	-EQUIPI ONCE). Ment power v The final ver	ALUES ARE IND NDOR IS SELEC	NCATIVE AND WI	ILL BE CON	FIRMED
	-FOR L TKOD1-	EGEND SHEETS DWG-A000-WG	SEE DRAWING NOO01;0002;00	5: 103;0004;0005;0 TIOXIDATION BA	0006 RRIFR	
	-NOTE -NOTE	2: HANDHOLE 3: SODIUM BIS	FOR TANK FLU	SHING ENTRATION 40%	RNER	
	-NOTE INCLUDE AND FL	4: ELECTROLY E ELEMENTS IN OWS.	SIDE THE MARK	ES PROCESS D (ED AREA. INCL	UDING PIPE	DIAMETER
	PIPE AF	RANGEMENTS, DLYTIC TECHNO	SUPPORTS AND LOGIES SCOPE.	CIVIL DESIGN	ARE OUTSIE	E B3
	-NOTE TECHN	5: ELEMENTS	CONNECTED T	H (*) ARE SUP O ELECTROLYTI	PLIED BY E	CLECTROLYTIC
	-NOTE	6: PRESSURE 7: VIBRATION	SAFETY VALVE	CANNOT BE IN:). STALLED IN	TUBING.
	-NOTE	8: TANK OUTL	ET AND EMPTY	TO BE FLUSHE	D WITH TAN	K BOTTOM.
			Electr	olytic		
			Cecili	lulugies		
		NOMINAL		NOMINAL	NOMIN	AL
		PIPE SIZE	DIAMETER DN	PIPE SIZE	DIAMET DN	ER
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		1/2"	DN15 DN25	10" 12"	DN25 DN30	0
		1 1/2"	DN40 DN50	14" 16"	DN35 DN40	0
		2 1/2"	DN65	18"	DN45	0
		4"	DN100	20	DN50 DN60	0
		5" 6"	DN125 DN150	28" 32"	DN70 DN80	0
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	B1	DDA SUBM	ISSION		M.P.	05/21
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Appendix A-22 Photo Records of Chemical Tank Outlet Control Valve and Filling Point (Page 1 of 4)

Chemical Building

A. Ferric Chloride – 3" Coupling Camlock for chemical filling



B. Sodium Hydroxide – 2-1/2" Coupling Camlock for chemical filling



C. Sodium Hypochlorite – 2" Coupling Camlock for chemical filling



Appendix A-22 Photo Records of Chemical Tank Outlet Control Valve and Filling Point (Page 2 of 4)

D. Fluorosilicic Acid – 1-1/4" Coupling Camlock for chemical filling



E. Sulphuric Acid – 1-1/2" Coupling Camlock for chemical filling



Appendix A-22 Photo Records of Chemical Tank Outlet Control Valve and Filling Point (Page 3 of 4)

OSCG Building

F. Hydrochloric Acid – 3/4" Coupling Camlock for chemical filling



G. Sodium Hydroxide $-2 \frac{1}{2}''$ Coupling Camlock for chemical filling



Appendix A-22 Photo Records of Chemical Tank Outlet Control Valve and Filling Point (Page 4 of 4)

H. Sodium Bisulphite – 1" Coupling Camlock for chemical filling



I. Sodium Hypochlorite – 2" Coupling Camlock for chemical filling



Appendix A-23 Bund Arrangement for Ferric Chloride Storage in Chemical Building



NOTES

- 1. DOUBLE BEND LOUVER WILL BE USED.
- HIGH AND LOW VENTILATORS FOR NATURAL VENTILATION COVERED INTERNALLY WITH METAL WIRE GAUZE OF NOMINAL APERTURE SIZE NOT GREATER THAN 12MM AND EXTERNALLY WITH NON-CORROBIBLE WITAL GRATINGS SHALL BE PROVIDED FOR THE STORE.

ABBREVIATION

H.R.	HOSE REEL
AL	NATURAL VENTILATION LOUVRE
ST	STAIR

RETAINING CAPACITY CALCULATIONS

RETA = LEN = 11.1	INING CAPACITY (A) IGTH x WIDTH x HEIGHT WITH PROTE 10 x 6.90 x 1.30 = 99.57 M3	ECTIVE COA	TING
SUMF = LEN = 0.50	P PIT CAPACITY (B) IGTH x WIDTH x HEIGHT 0 x 0.50 x 0.50 = 0.13 M3		
PLAT = LEN HEIGI = 7.04	FORM VOLUME (C) AGTH x WIDTH x HEIGHT + BEAM WID HT 4 x 1.80 x 0.15 + 0.3 x (6.74+1.40) x 0.45	TH x BEAM 5 = 3.00 M3	LENGTH x BEAM
PLINT = LEN = 8.60	TH VOLUME (D) IGTH x WIDTH x HEIGHT 0 x 3.90 x 0.20 = 6.71 M3		
COLU = COI = (0.4 = 0.27	JMN VOLUME (E) LUMN AREA x HEIGHT -0 x 0.20 + 0.20 x 0.20 + 0.20 x 0.10 + 0. 7 x 1.30 = 0.35 M3	40 x 0.10 + (0.30 x 0.30) x 1.30
VOLU CHEN	IME OCCUPIED BY EQUIPMENT (F) (3 MICAL) 3 x 85.58 = 2.57 M3	% OF TOTA	L QUANTITY OF
TOTA = (A) = 99.5	AL RETAINING CAPACITY + (B) - (C) - (D) - (E) - (F) 57 + 0.13 - 3.00 - 6.71 - 0.35 - 2.57 = 87.	07 M3 > 42.	79 x 2 = 85.58 M3
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Appendix A-24 Bund Arrangement for Sulphuric Acid Storage in Chemical Building



Appendix A-25 Bund Arrangement for Fluorosilicic Acide in Chemical Building



Appendix A-26 Bund Arrangement for Sodium Bisulphite Storage in Chemical Building



BINNIES

Appendix A-27 Bund Arrangement for Sodium Hydroxide in Chemical Building



Appendix A-28 Bund Arrangement for Sodium Hypochloride Storage in Chemical Building





Appendix A-29 Bund Arrangement for Sodium Bisulphite Storage in OSCG Building



Appendix A-30 Bund Arrangement for Hydrochloric Acid Storage in OSCG Building



Appendix A-31 Bund Arrangement for Sodium Hydroxide Storage in OSCG Building





Appendix A-32 Bund Arrangement for Sodium Hypochlorite Storage in OSCG Building





Appendix A-33 Photo Records of Chemical Storage Bund (Page 1 of 3)

Chemical Building:

Ferric Chloride Storage Bund



Hypochlorite Storage Bund



Sodium Bisulphite Storage Bund





Fluorosilicic Acid Storage Bund



Sulphuric Acid Storage Bund

Sodium Hydroxide Storage Bund



Appendix A-33 Photo Records of Chemical Storage Bund (Page 2 of 3)

OSCG Building



Hydrochloric Acid Bund Area

Sodium Hydroxide Bund Area







Appendix A-33 Photo Records of Chemical Storage Bund (Page 3 of 3)

Sodium Bisulphite Bund Area





Sodium Hypochlorite Bund Area

Rev. B4

Approved BC

TBD

17 JUN 2021

30 APR 2020

25 FEB 2020

13 NOV 2020

Date

Appendix A-36 Photo Records of Sump Pits

Chemical Building:

OSCG Building:

Appendix A-37 Trench HCl Pipe Alignment in DP1

| Water Supplies Department

Appendix A-38 HCl Pipe Alignment in OSCG Building

| Water Supplies Department

PRINCIPAL DATUM (HKPD).

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	T1GCM46 BB002		5.3		
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	T1GCM40 BB002		9.6	5	
	T1GCM42 BB001		11.3		
	T1GCM42 BB002		11.3	3	1
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E	T1GCM38 BB002	19.11			
E	T1GCM38 BB003		19.1	1	
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	T1GCM10 BB002		5		
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水務署 Water Supplies Department

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ON SITE CHLORINE GAS PLANT BUILDING

F0 JB 9-12-2022 FSI/314 DRAWING ©COPYRIGHT RESERVED

Appendix A-39 Double Containment HCl Pipe

| Water Supplies Department

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KEY PLAN	DWG AREA								
Approved This plan is in accordan	ce with the								
Dangerous Goods Ordinance and is app of Dangerous Goods within any app Goods Store however is subject to the the recommendations for the gr which will be issued separately by let	roved. The storage roved Dangerous compliance with ant of approval ter.								
15 FEB 2023 certificu	(O Mgao-tin) AP Fire Services								
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Designer)								
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Drowing 1880 ON SITE CHLORINE GAS PLANT BUILDING DOUBLE CONTAINMENT PIPING									
Drawing no.	Rev.								
Drawn LA G	Checked Approved								
Scale 1:100	Status PRELIMINARY DESIGN								
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Appendix A-40 HCl Bund Room

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Appendix A-42 Hoses and Couplers for Chemical transfer (Page 1 of 2)

Sizes of coupling cam locks for chemical filling at OSCG and Chemical Buildings are summarized as below:

<u>Chemicals</u>	<u>OSCG Building</u>	<u>Chemical</u> <u>Building</u>		
Sodium hypochlorite	2"	2"		
Sodium hydroxide	2-1/2"	2-1/2"		
Sodium bisulphite	1"	N/A (powder)		
Fluorosilicic acid	N/A	1-1/4"		
Ferric chloride	N/A	3"		
Sulphuric acid	N/A	1-1⁄2"		
Hydrochloric acid	3/4"	N/A		

Chemical Building

A. Ferric Chloride Filling Point – 3" Coupling Camlock for chemical filling



B. Sulphuric Acid Filling Point – 1-1/2" Coupling Camlock for chemical filling



Appendix A-42 Hoses and Couplers for Chemical transfer (Page 2 of 2)

OSCG Building

C. <u>Hydrochloric Acid Filling Point – 3/4</u>" Coupling Camlock for chemical filling



Appendix A-43 Warning Signs (Page 1 of 4)

Chemical Building

A. Ferric Chloride Filling Point – <u>3</u>" Coupling Camlock for chemical filling



B. Sodium Hydroxide – 2-1/2" Coupling Camlock for chemical filling



C. Sodium Hypochlorite – 2" Coupling Camlock for chemical filling



Appendix A-43 Warning Signs (Page 2 of 4)

D. Fluorosilicic Acid – 1-1/4" Coupling Camlock for chemical filling



E. Sulphuric Acid – 1-1/2" Coupling Camlock for chemical filling



OSCG Building

F. Hydrochloric Acid – ¾" Coupling Camlock for chemical filling



Appendix A-43 Warning Signs (Page 3 of 4)

G. Sodium Hydroxide – 2-1/2" Coupling Camlock for chemical filling



H. <u>Sodium Bisulphite – 1" Coup</u>ling Camlock for chemical filling



Appendix A-43 Warning Signs (Page 4 of 4)

I. <u>Sodium Hypochlorite – 2" Coupling Camlock for chemical filling</u>



Appendix B Design Requirements and Measures for CO₂ Storage

Appendix B-1 Actual CO₂ System Layout and Tank Capacity



Appendix B-2 Photo Record of CO₂ Tanks in DP1



Appendix B-3 Specifications of CO2 Tanks in DP1 (Sheet 1 of 2)



Appendix B-3 Specifications of CO2 Tanks in DP1 (Sheet 2 of 2)









Appendix B-4 P&IDs of Remineralisation CO2 Storage Tanks and Related Systems (Sheet 2 of 5)





Appendix B-4 P&IDs of Remineralisation CO2 Storage Tanks and Related Systems (Sheet 3 of 5)









BINNIES



Appendix B-4 P&IDs of Remineralisation CO2 Storage Tanks and Related Systems (Sheet 5 of 5)

BINNIES

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	NOTES: -INFER O KOCH-OL-HOUD-ARECOM PROCESS CALCILATIONS & IOL-PART SIZING REMAINER, ICON TOR FURTHER INFORMATION OF PROCESS PRAMETERS. -OUHMANT POWER CONSUMPTION IS LUSTRATIVE FINA. WHILES TO SE OVEN WHITE IN LUSTRATIVE FINA. -FOR LESHO SHETTS SEE DRAWNS: INFORM-FINA-DRAW-OWN COMPONENCIAL OF DRAWSED. -FOR LESHO SHETTS SEE DRAWNS: INFORM-FINATION COMPONENCIAL OF DRAWSED. -FORT 1: CALIFIENTS WIT FINA. VINDOR INFORMATION.
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	DESIGN, BUILD AND OPERATE FIRST STAGE OF TSEUNG KWAN C DESALINATION PLANT Drawley Litle PROCESSIAND INSTRUMENTATION DIAGRAW REVINERALIZATION CO2IDOSING SYSTEM Drawley tea TKODT - PID- 1000 - APE0002 01 Provinci Diage Drawley Approve
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Appendix B-5 P&ID of CO₂ Road Tanker

代号																
HCV-1	液相充液	阀	MECA-INOX #PS4LSWVI050	2"	1											
HCV-2	气体回气	阀	MECA-INOX #PS4LSWVI025	1"	1											
HCV-3	液体出口	阀	MECA-INOX #PS4LSWVI025	1"	1	1										
HCV-6	手动排放	阀	HEROSE#01321.2533.001	1"	1]										
HCV-7	气相针型	阀	REGO #CMM250A B31.3	1/4"	1]										
HCV-8	液相针型	阀	REGO #CMM250A B31.3	1/4"	1]										
HCV-9	平衡针型	阀	SWAGELOK #B-1RM4-SC11	1/4"	1											
HCV-10	泵进液的	划	MECA-INOX #PS4LSWVI050	2"	1											
HCV-11	泵出口阀	因	MECA-INOX #PS4LSWVI025	1"	1	1										
HCV-12	压力出液	阀	MECA-INOX #PS4LSWVI025	1"	1											
HCV-13	回流阀		MECA-INOX #PS4LSWVI025	1"	1											
HCV-14,15	排压阀		REGO #CMM250A B31.3	1/4"	2											
HCV-17,18,19	排残阀		MECA-INOX #PS4LSWVI015	1/2"	3								\mathbf{h}	101-10	<u>¥</u> —1 <u>Х</u> н Хнсv-14	Хнсv-15
HCV-20	泵体回流	阀	REGO#C009464DAS PI-MARK	3/8"	1		1				C 1-1/	2"	s	SD-2		
HCV-21,22	溢满阀		MECA-INOX #PS4LSWVI015	1/2"	2						B 1" F 1/4" G 1/2"				HCV-7	
HCV-23	三通切换	阀	BESTOBELL#CJF60SS7CLE1T	DN32	1						1/2"			HCV-22 *	- HCV-9	\$
HCV-25	液相根部	阀	MECA-INOX #PS4LSWVI050	2"	1						E 1/4	"			HCV-8	\square
HCV-99	规管截止	阀	HOKE 4111L2B BRS 1/8MPTX1/8FF	1/8"	1						D 2"				-	нс
TC-1	真空规管	音	HASTINGS 1415671S #DV-6	1/8"	1									XH3 AC-1 XHCTC-1	∑нсv-10 _∎ тsv-	8 D
VAC-1	抽真空闲	划	LANSHI #ZK-30/40-1Q(KF40)	1-1/2"	1								R.Y-		LA-	PUMP
TSV-1,2,3	安全阀		REGO #PRV9432T450	1/4"	3									L		
TSV-8,9,10	安全阀		REGO #PRV9432T450	1/4"	3										ł	LV-12
PSV-1A,B	安全阀		HEROSE #06388.1510.6040 UV	1"	2											
PSV-2A,B	安全阀		HEROSE #06388.1510.6040 UV	1"	2											
PI-1	储罐压力	表	WKA #233.50 1/4MPT W/ PANNEL	0-4Mpa	1											
PI-2	泵出口压力	力表	WIKA #232.50 1/4MPT W/ PANNEL	0-4Mpa	1											
LI-1	液位计	· · · · ·	WIKA #712.15 W/PANEL	0-2500MM	1											
PUMP	泵		PUMP CO2 R83-316H4BM-0405T1-	TEIKOKU	1											
C-1,3	CGA接头	, ,	YCLB #CGA-CO-40-001	1-1/2"	2									<u> </u>		
C-2	CGA接头	< ¹	YCLB #CGA-CO-25-001	1"	1									-		
M-1	流量计		FLOWCOM 3000 #SWM33.4*	1"	1		标记 払 社	火数	\$ X	更改文件	号 4	签字	年月日		-)1	<i>a</i> . =
DP	压差变送	器	ROSEMOUNT 3051CD3A02A2BH2	2	1		校对			RME	ītu —				7北	重重
RTD	温度传感	器	BURNS#200A 10BN035		1		<u> 审核</u>				Æ			#	而	螢

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Appendix B-6 Pressure Relief System of Inner and Outer Vessel of Insulated Tank and Carbon Dioxide Road Tanker

Pressure relief system of the inner vessel is as below:



Characteristics :

- Two sets of relief valves, one duty and one standby. Such design allows annual calibration without interrupting the system.
- 2. There is a 3-way diverter valve to switch between duty and standby. Design of valve ensure opening at either side (ie. Either to left or right). There will not be accidental closing of both streams.
- 3. Each side consists of two relief valves in two settings, usually at 22 barg and 24 barg. The two stage design allows double protection. In case pressure rises too quickly that the first stage valve cannot release the pressure, there is the second stage relief valve for protection.

Above designs fulfills the requirement of Table 1 - List of design requirements / measures for chlorine and carbon dioxide storage extracted from Annex 13L of the EIA Report (Register No. AEIAR-192/2015))-Item 2.4.

At outer vessel of vacuum insulated tank, there will be a burst disc plate, usually set at 1.0 barg. This is for protection of outer vessel. The design fulfills requirement of Environmental Permit Clause 2.4 part 2.

Appendix B-7 Photo Record of Pressure Relief Valves on CO₂ Tank



Appendix B-8 Details of Trycock Valve

Globe Valves Type 01321 - Globe Valve

Cryogenic-Globe and Globe/Check Valves, PN50 (DN150=PN40)

Stainless steel body and bronze topwork " live loaded " gland packing " cleaned and degreased for oxygen service " Part No. 01321.X.001* (H = 270mm) Part No. 01321.X.002* (H = 370mm) Part No. 01321.X.501* (H = 270mm) Globe/Check Valve Part No. 01321.X.502* (H = 370mm) Globe/Check Valve *Butt weld connection for stainless steel pipes acc. to ISO 1127 or ASTM A312 Part No. 01321.X.0014 (H = 270mm) Part No. 01321.X.0024 (H = 370mm) Part No. 01321.X.5014 (H = 270mm) Globe/Check Valve Part No. 01321.X.5024 (H = 370mm) Globe/Check Valve Socket weld connection for stainless steel pipes acc. to ISO 1127 or ASTM A312 Available options - on request only: · Welded stainless steel stubs acc. to ISO 1127 or ASTM A312 - length FF + 200mm · Extension H up to 900mm · Valve with control disc (tapered design) Further pipe wall thicknesses

Applications:

Approved for air gases, vapours and cryogenic liquefied gases incl. LNG. Working temperature: -196°C / -321°F (77K) up to +120°C / +248°F (393K)

Mat	terials	DIN EN	ASTM
1	Body	1.4308	A 351 CF8
2	Valve seal up to DN50	PTFE / Ca	rbon filled (25%)
2a	Valve seal from DN65	PTFE	
3	Disc	CW614N	B 283 UNS C38500
4	Bonnet gasket	PTFE	
5	Headpiece	CC493K	B 505 UNS C93200
6	Bolts	1.4301/A2	A 194 B8
7	Elongation tube	1.4541	A 213 TP 321
8	Stem	1.4301	A 276 Grade 304
9	Gland packing	Graphite /	PTFE
10	Gland nut	CW614N	B 283 UNS C38500
11	Handwheel	Aluminium	alloy
12	Spring	CW452K	B 159 UNS C51900

Standard marking acc. to Pressure Equipment Directive 2014/68/EU (PED).



Type 01321 - Standard design	recnni	cal da	ta											
Nominal size	DN	10	15	15	20	25	32	40	40	50	65	80	100	150
Dimension code	.X.	1012	1517	1521	2026	2533	3238	4042	4048	5060	657x	8088	0114	0168
Face-to-face dimension	FF	70	85	85	100	115	115	130	130	155	205	245	280	400
Height	н		270mm	or 370)mm								370	420
Outside pipe-Ø ISO 1127	RA	12.0	17.2	21.3	26.9	33.7	38.0	42.4	48.3	60.3	76.1	88.9	114.3	168.3
Wall thickness pipe ISO 1127	а	1.0	1.6	2.0	2.0	2.0	2.0	2.0	2.0	2.0	2.6	3.2	6.0	7.1
Outside pipe-Ø ASTM A312	RA	13.72	17.15	21.34	26.67	33.40	-	42.16	48.26	60.32	73.02	88.90	114.30	168.27
Wall thickness pipe ASTM A312	a o	dimens	ions ac	c. to S	10 or S	40								
Socket depth	b	6	10	10	13	13	-	13	13	16	16	16	20	20
Handwheel-Ø	В	100	100	100	100	100	125	125	125	125	200	250	315	360
Wrench size across flats	S1	7	7	7	7	7	10	10	10	10	10	10	12	15
Wrench size across flats	S ₂	30	30	30	30	30	36	36	36	36	36	36	41	41
Weight	ca. kg	1.4	1.65	1.7	2.1	2.4	3.3	4.7	4.7	7.2	12.7	17.0	24.5	54.0
Kvs-Value	m ³ /h	1.6	3.8	4.3	6.7	11.5	14.0	20.6	22.6	37.1	71.1	104.0	170.0	350.0
Cv-Value	gal/mir	1.9	4.4	5.0	7.8	13.4	16.2	23.9	26.3	43.2	82.7	120.9	195.2	401.8

CE

Dimensions in mm. Compliance of tightness requirements acc. to EN 1626 for DN150 up to 20 bar differential pressure. In the range of >20-40 bi 350-700ml (1 bar, 20°C [68°F]) are reached.

HEROSE GMBH Phone +49 4531 509-0 Fax +49 4531 509 120 info@herose.com www.herose.com





Edition 2018-04

Appendix B-9 Photo Record of Trycock Valve



Appendix B-10 Photo Record of Security Fence



Appendix B-11 Inspection Report for Vaporizers (Sheet 1 of 7)

INFO INSPE	RME DE	INSPE PORT	CCION	Gacciona	GIS CLOBAL INSPECTION ERRYICES WWW.ginabetlionservices.com
Proyecto: Project:	FIRST ST PLANT	TAGE OF	TSEUNG KWA	AN O DESALINATION	Report Page: Pag.1 /6 Ref. Proj. HK01C1 (P.019)
Cliente: End User:	ACCIONA	AGUA			Inspec. date: 2021.08.04 Report date: 2021.09.29
GENERAL:		I			
INFORME REPORT:		IRn1_P.01 CRYOQUI (HK01C1-0) IR1_Rev02)	9_190 CO2 System P_Rev02 0-WQ-A13LC -LINDE-	NOTIFICACION INSPECCION INSPECTION NOTIFICATION:	HK01C1-A13LC CO2 SYSTEM_Notice_for_inspectio n_ LINDE- 1
SUMINISTR SUPPLIER:	RADOR:	LINDE HK	O LTD.	PEDIDO/ SUB-PEDIDO No.: ORDER / SUB-ORDER No.:	HK01C1-A13LC
LUGAR INS PLACE OF IN	SPECCION: NSPECTION:	CRYOQUI LEIDIAN T COUNTY, ZHEJIANG	P CHINA CO., LTD OWN, DEQING HUZHOU CITY, PROVINCE	PROGRAMA (PPI) No.: TEST PLAN (ITP) No.:	TKOD1-ITP-A000-AGN9701
ASISTENTE ATTENDANT	ES: 'S:	 Zhajinhe Chenyue 	(obo Acciona) xin	ESPECIFICACION No.: TECH. DATA SHEET No.:	TKOD1-TDS-H000- AME0006_Rev C1 (10/02/21)
SUPPLY:		2 X VAP	ORIZER		
INSPECTIO	N:	•			
OK NOT	NA ITP No.			COMENTARIOS / COMMENTS	;
		Material ce	rtificates		
		Pressure te	est certificate		
		visual and	dimensional check	Ph to . t	
	4	Final dossi	er of manufacturing qua	ality control	
		Acceptance	e Note		
	OK: performed	& correct	NOT:requested by ITP but No	I performed /Performed but Not correct N	IA: Not Applicable acc. ITP
ESTADO I INSPECTION	NSPECCION STATUS:			. PARCIAL / PARTIA	PROCUREMENT: 100 % MANUFACTURING: 100 % TESTING: 100 %
RESULTA OVERALL INS	DO INSPECC SPECTION RESUL	T:	SATISFACTORI SATISFACTORY	A DESVIACION MENO MINOR DEVIATIONS	R NO SATISFACTORIA NOT SATISFACTORY
	-				
Realizado p Submitted by	GIS inspector):	GIS):		Certificación (sólo TPI): Certification (only TPI):	
		Zhajir	yee		
Fdo./Sign: Z	'ha Jinhe GIS li	nspector obo	Acciona		
TIPO INSPE	ECCION:			SPI / SECOND PARTY	

INFO INSPE	CTION RE	E INSPEC	CION	acciona	2	GI	GLOBAL INSPECTION SERVICES TIONSOFTICES.com	7		
Proyecto: Project:	FIRST	STAGE OF T	SEUNG KWAN	O DESALINA	TION	Report Page:	: Pag.2 /	8		
Ollowing	PLANI					Ref. Proj.	HK01C1 (P. 2021 08.04	.019)		
Cliente: End User:	ACCION	A AGUA				Report date:	2021.09.29	_		
1.0	DESCRIP	CION DETAL	LADA EQUIPO / DE	TAILEDEQUIP	MENT DE	SCRIPTIO	N:			
2 X VAI - - - - -	ORIZER: Model: CV4 Serial No.: (Tag No: T1 Fluid: CO2 MAWP: 31E	00-CO2 67320101 / 67320 GKL01 AH001 / 1 3ARG	0102 T1 GKL01 AH002							
2.0	DOCUME	ENTOS DE REI	FERENCIA / APPLI	CABLE DOCUM	IENTATIO	DN:				
-	Datasheet: Drawings: 2 Purchase o Nameplate Vendor's D	TKOD1-TDS-H00 225180361 (22/04 irder: HK01C1-A vaporizer IS vaporizer)0-AME0006_Rev C1 (* I/2021) 13LC (19/03/2021)	10/02/21)						
3.0	DETALL	E TRABAJOS	REALIZADOS / DE	TAIL OF INSPE	CTION A	CTIVITIES	:			
The ins results a ITP 1 / I The fac the requ Result: ITP 2 / I Pressu	pector arrived are as follows Review of Ma tory submitte tirements of t satisfactory Review of Pr re test witne	d at CRYOQUIP aterial Certificate d relevant raw ma technical specifica ressure test certi	China Co., Ltd on Augu es aterial quality certificate ations and EN1024 star	ust 4, 2021 to insp to our inspectors idards.	ect the two	o vaporizers.	The inspection	on et		
5	pecification	requirements		Measure	ed					
E	quipment	Test pressure	essure Pressure gauge No Test medium Pressure holding time Test pressure							
VA	PORIZER-1	44 Barg (pneumatic)	1810P-32681-10223 1810P-32681-10224	compressed air	≥60m	nin :	3.4MPa			
VA	APORIZER-2 44 Barg 1810P-32681-10229 compressed air ≥60min 3.4MPa									
	Remark no specification carried out i 34 barg. The that indicate that indicate test report h	.1-closed: inspect , which requires the n accordance with e measured field is that the test pre- is the 34 Barg is, so has been reviewed	ctor asked the factory the pressure test to be h the requirements of th pressure test is incons assure must be 44 barg so this remark is closed.	to conduct the pro- 44 barg (pneumal he drawing. The pr- istent with the teo is not a document Also pending to re-	essure tes tic). The fa ressure tes hnical spe t approved eview press	t according t ctory indicate st required by cifications. T by Acciona, sure test certi	to the technic ad that this way the drawing he specification but the drawing ficate. Pressu	al is on ng re		

Explanatory note: The pressure test was carried out according to GB / 151-20141, holding time: 30 minutes.

Appendix B-11 Inspection Report for Vaporizers (Sheet 3 of 7)

INFOI INSPEC	RME DE INSPECCION	acciona	R		GLOBAL INSPECTION SERVICES nservices.com
Proyecto:	FIRST STAGE OF TSEUNG KW	AN O DESALINA	TION	Report Page:	Pag.3 /6
Project:	PLANT			Ref. Proj.	HK01C1 (P.019)
Cliente:				Inspec. date:	2021.08.04
End User:	ACCIONA AGUA			Report date:	2021.09.29
Design s	tandard is ASME Section VIII Div 1: 2019 E	d, in which ASME UG-100) code req	uires that the	pressure test

Design standard is ASME Section VIII Div 1: 2019 Ed, in which ASME UG-100 code requires that the pressure test needs enough time, and the factory shall issue the test report according to 30 minutes.

However, during the on-site witness, the pressure holding time of the factory actually adopts the test pressure is 1 hour.

Result: satisfactory

ITP 3 / Visual and dimensional check

The appearance of the two carburetors was inspected, and the external surface was free of scratch and collision. The overall appearance was qualified.

Inspector checked the dimensions of the two vaporizers.

Some dimensions differ from the drawing but are within the specified tolerances.

VAPORIZER-1 (TAG: T1 GKL01 AH001 / S/N: 67320101):

	Equipment	t size (mm)	Total length (mm)	Support size (mm)		Bolt hole spacing (mm)		
Drawing requirements	L=1699	H=1699	L=7044	L=1305	H=1333	L=848	H=1130	
Actual measurement	L=1706	H=1705	L=7058	L=1306	H=1335	L=854	H=1135	

VAPORIZER-2 (TAG: T1 GKL01 AH002 / S/N: 67320102):

	Equipment	t size (mm)	Total length (mm)	Support size (mm)		Bolt hole sp	bacing (mm)
Drawing requirements	L=1699	H=1699	L=7044	L=1305	H=1333	L=848	H=1130
Actual measurement	L=1708	H=1707	L=7055	L=1305	H=1334	L=854	H=1135

Result: satisfactory

ITP 4 / Review of final Dossier of manufacturing quality control

Pending to review final quality dossier.

The following documentation has been reviewed:

- Material certificates
- Cleaning certificate
- Certificate of compliance
- Pressure test reports

Result: satisfactory

Appendix B-11 Inspection Report for Vaporizers (Sheet 4 of 7)

INFO	RME DE INSPECCION		GLOBAL INSPECTION SERVICES aservices.com
Proyecto:	FIRST STAGE OF TSEUNG KWAN O DESALINATION	Report Page:	Pag.4 /6
Project:	PLANT	Ref. Proj.	HK01C1 (P.019)
Cliente:		Inspec. date:	2021.08.04
End User:	ACCIONA AGOA	Report date:	2021.09.29
4.0	INSTRUMENTACION UTILIZADA/ USED TEST EQUIPMENT:		

Туре:	Model / Identification:	Calibration status:
Tape measure	0-7000mm	N/A
Pressure gauge	0-6MPa	13/07/2021
Pressure gauge	0-10MPa	13/07/2021
Pressure gauge	0-10MPa	13/07/2021

5.0

DESVIACIONES - PENDIENTES / REMARKS - PUNCH LIST:

OBSERVACIONES / DESVIACIONES MENORES:

REMARKS / MINOR DEVIATIONS:

Remark no.1-closed: inspector asked the factory to conduct the pressure test according to the technical specification, which requires the pressure test to be 44 barg (pneumatic). The factory indicated that this was carried out in accordance with the requirements of the drawing. The pressure test required by the drawing is 34 barg. The measured field pressure test is inconsistent with the technical specifications. The specification that indicates that the test pressure must be 44 barg is not a document approved by Acciona, but the drawing that indicates the 34 Barg is, so this remark is closed. Also pending to review pressure test certificate. Pressure test certificate has been reviewed.

NO CONFORMIDADES / DESVIACIONES MAYORES:

NON CONFORMITIES / MAYOR DEVIATIONS:

N/A

Appendix B	-11 Inspection Report for V	aporizers (Sheet 5 of 7)			
INFO	RME DE INSPEC	CION		GIS	GLOBAL INSPECTION SERVICES nservices.com
Proyecto:	FIRST STAGE OF T	SEUNG KWAN O DESALINA	ΓΙΟΝ	Report Page:	Pag.5 /6
Cliente:	PLANT			Ref. Proj.	HK01C1 (P.019) 2021.08.04
End User:	ACCIONA AGUA			Report date:	2021.09.29
6.0	ANEXO FOTOGRAFICO)/ PICTURE APENDIX:			
A) GE	ENERAL VIEW & IDENTIFICATION				
			1	A 601-15 600 10	
	Pic.1: Workshop	Pic,2: Appearance inspection (ITP no.3)	Pic	.3: Appearance insp	ection (ITP no.3)
				H H H H	
Pic.4: A	ppearance inspection (ITP no.3)	Pic.5: Appearance inspection (ITP no.3)	Pic	.6: Appearance insp	ection (ITP no.3)
	B) TESTS				
Pic.7:	Test 1 (ITP no.2) pressure test	Pic.8: Test 2 (ITP no.2) pressure test	Pi	ic.9: Test 3 (ITP no.2	?) pressure test
Dia 44:	Tet 4 (ITP ng ²) researce test	Pir 11' Test 5 //TP no 3) property test		42: Test 6./ITD ex	2) presure fact
Pic,10:	rest 4 (TP no.2) pressure test	PIC.11: Test 5 (TEP no.2) pressure test	Pie	C, 1Z: 16ST 6 (ITP NO,	z) pressure test

Appendix B-11 Inspection Report for Vaporizers (Sheet 6 of 7)





	15 16 REV DESCRIPTION	<u>17</u> ωπ	AUTHOR	2
	- -			ě.
				225180361
	APPROVED WITH COMMENTS NOT APPROVED. ADD INFORM FOR INFORMATION	IATION		2407
	THIS APPROVAL DOES NOT RELEASE THI FULFILLMENT OF CONTRACT OBLIGATION	e NS		-
	DATE 21-06-21 SIGNATURE T.O			2
H J X DAT LES (UR - COULSESE,), f	VA Adhesive Anch with HAS anchor ro 210 A: UNITS DESIGNED TO ASME SI SURE VESSEL CODE, NO U S CO2): 195.5 TO +65.5°C. 2): 195.5 TO +		VIII	CAD ORIGINATED DRAWING. REVISION UPDATES RESTRICTED TO CAD SYSTEM ONLY. NO MANUAL UPDATES.
and B	OUTLINE MODEL CV400-CO AMBIENT VAPORIZ 7X733 800 10 225180 RET. SOALE 1/1 NEXHT 59 SEE 3	02 ER 0361	OF 1 PARTS LE	57

Appendix B-12 CO₂ Tanker License

	Licence No. V000001190 牌照编號
	THE GOVERNMENT OF THE HONG KONG SPECIAL ADMINISTRATIVE REGION 香港特別行政區政府 Dangerous Goods Ordinance Chapter 295 Section 6 and Section 9 危險品條例 第二百九十五章 第六條及第九條 LICENCE FOR THE CONVEYANCE OF DANGEROUS GOODS IN CATEGORY 2/5 BY VEHICLES 載運第二/五類危險品車輛醉照
. 6 .	 Name of Licensee 持牌人姓名Linde HKO Limited Address of Licensee 持牌人地址
	 Dangerous Goods:- (Classification): Category
	 Valid period of this licence 本牌照有效日期26/05/2021 - 25/05/2022 This licence is issued subject to the conditions specified overleaf. 本牌照係依照後頁之規餘而發
	(CHAN Wai-kay) for Director of Fire Services, Licensing Authority. 消防處處長(登牌當局) (陳偉基(行)
	FSD Ref. (29) in 11/12995(1) 消防威檔案編號 FS 272 (Rev. 4/2012)

Appendix B-13 Separation Distance from Slope Toe from BIM Model



Appendix B-14 Photo Record of 1.5 m High Barrier Behind CO2 tank



Appendix C Separation Distances Between Major Facilities in DP1

Appendix C Separation Distances Between Major Facilities in DP1





Our Ref: PL-202405006



Date: 3 May 2024

AJC Joint Venture 5/F, Tower A, Manulife Financial Centre, 223-231 Wai Yip Street, Kwun Tong, Kowloon, Hong Kong

Attn: Mr. Brian Kam

Dear Sir,

Contract No. 13/WSD/17 Design, Build and Operate First Stage of Tseung Kwan O Desalination Plant Certification of Audit Report on Measures for Mitigating Hazard to Life (Issue 3)

We refer to the revised Audit Report on Measures for Mitigating Hazard to Life (Issue 3) issued on 30th April 2024 for the captioned project.

We have no further comment and hereby certify the captioned submission in accordance with Condition 2.20 of Environmental Permit EP-503/2015/B and Further Environmental Permit FEP-01/503/2015/B.

Yours Faithfully, For and on behalf of Acuity Sustainability Consulting Limited

Jacky C. H. Leung Environmental Team Leader


Our ref.: LES/J2024-01/CS/L011 Date : 3 May 2024

By Post and Email

Water Supplies Department New Works Branch Consultants Management Division 6/F, Sha Tin Government Offices, 1 Sheung Wo Che Road, Sha Tin, New Territories

Attn: Mr. Sam Hui/ Mr H L Lai

Dear Sirs,

Independent Environmental Checker (IEC) for Construction and Operation of the First Stage Desalination Plant at Tseung Kwan O (Quotation Ref. No. TKO1/IEC/003)

Verification of Audit Report on Measures for Mitigating Hazard to Life

We refer to the revised Audit Report on Measures for Mitigating Hazard to Life (Issue 3) for the captioned project prepared by Binnies Hong Kong Limited.

We have no further comment and hereby verify the captioned report in accordance with Condition 2.20 of Environmental Permit EP-503/2015/B and Further Environmental Permit FEP-01/503/2015/B.

Yours sincerely, For and On Behalf Of Lam Environmental Services Limited

Serena Shek Independent Environmental Checker

Encl.